Pulsed power corona discharges for air pollution control

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Pulsed Power Corona Discharges for Air Pollution Control
Erwin H. W. Smulders, Bert E. J. M. van Heesch, and Sander S. V. B. van Paasen

Abstract—Successful introduction of pulsed corona for industrial purposes very much depends on the reliability of high-voltage and pulsed power technology and on the efficiency of energy transfer. In addition, it is of utmost importance that adequate electromagnetic compatibility (EMC) is achieved between the high-voltage pulse source and the surrounding equipment.

Pulsed corona is generated in a pilot unit that produces narrow 50 MW pulses at 1000 pps (net average corona power 1.5 kW). The pilot unit can run continuously for use in industrial applications such as cleaning of gases (100 m³/h) containing NO or volatile organic compounds (VOC’s) or fluids (e.g., waste water). Simultaneous removal of NO and ethylene to obtain clean CO₂ from the exhaust of a combustion engine was tested at an industrial site.

Various chemical processes, such as removal of toluene or styrene from an airflow are tested in the laboratory. We developed a model to analyze the conversion of these pollutants. To examine the discharges in the reactor we use current, voltage, and E-field sensors as well as a fast charge-coupled device (CCD) camera. Detailed energy input measurements are compared with CCD movies to investigate the efficiency of different streamer phases.

Advantages of pulsed corona treatment are: simultaneous removal of several pollutants, high destruction efficiency, no demands on temperature and pressure, insensitive to contamination, no damage from high loads, widely applicable, simply installed, compact, little service, small scale, and no additives.

With respect to electromagnetic compatibility (EMC), methods have been developed to effectively suppress interference, in a systematic and reproducible manner, by appropriate guidelines and rules for the layout [6], [7]. Sensitive apparatus for chemical analysis should operate reliably close to the pulse source. Computers and networks in close vicinity and in the surrounding building should remain undisturbed.

II. PULSE SOURCE AND CORONA REACTOR

The pulsed corona unit produces 100 kV pulses (10 ns risetime, 200 ns wide) at a maximum rate of 1000 pulses per second. An overall efficiency of 40–70% was obtained for the energy transfer from mains AC power to corona energy. The mean time between failures for the complete apparatus was approximately 100 h; it was limited by the problem of partial discharge growth toward breakdown in the cable of the transmission line transformer. After improvement of this part, failureless operation now passed the 350 h and is planned to reach 2500 h as testing continues.

Fig. 1 gives an overview of the layout and main components of the pulse source. The corona reactor is placed on top of the main EMC casing. For the production of the high-voltage pulse we use three stages: two resonant circuits coupled by a pulse transformer, followed by a transmission line transformer (TLT) as a third stage [8]. Each stage compresses the pulse duration and raises the pulse amplitude.
The first resonant circuit ($C_0, L_1, C_1$) at, respectively, 26 mF, 27 $\mu$H, 12 $\mu$F) and part of the second resonant circuit ($C_2, L_2 = 28 \mu$H) are at the low-voltage side (up to 750 V) of the pulse transformer. The pulse transformer (10:600) and the high-voltage capacitor $C_{HV}$ (6 nF) to which it is connected complete the second circuit. This capacitor is pulse charged by the resonant circuits in 40 $\mu$s to a level of 25–35 kV. The low inductance spark gap (50 $\mu$H, coaxial with $C_{HV}$) discharges $C_{HV}$ into the TLT. Diode $D_1$ (with snubber $Z_1, Z_2$) holds the voltage at $C_{HV}$. Although the spark gap is free running, an automatic triggering, derived via 2 M$\Omega$ from the voltage reversal at the transformer secondary is added to avoid misfiring. The transformer voltage reversal is damped via diode $D_2$ and the 28 k$\Omega$ resistor.

After each high-voltage pulse, part of the energy returns to the low-voltage resonant circuits. This surplus of energy depends on the actual breakdown voltage of the spark gap. Depending on the value of this energy, the $V_{C_1}$ control system first dumps part of the previously stored energy of buffer capacitor $C_2$ (20 $\mu$F). Next the surplus energy is shared by $C_2$ and $C_3$ for partial reuse in the next pulse.

The reliability of the spark gap is excellent, after $10^9$ pulses (total transferred charge 200 kC), only minor electrode wear is visible. The gap has to be flushed continuously with air (30 Nm$^3$/h typically). The spark gap transfers the energy of capacitor $C_{HV}$ to the TLT: four coaxial cables, each 50 $\Omega$ and 20 m long (RG214 later replaced by RG218 of 12 m length). We found that four cables is an excellent number with respect to amount of cable, impedance match, and voltage gain. At no load the TLT multiplication ratio is approximately 5.5, resulting in a peak output voltage of 160 kV (10 ns rise time). Loaded by corona the voltage is 100 kV.

Measured voltage and current and calculated power and energy are shown in Figs. 2 and 3. The corona power is the
calculated product \((VI)\) of the measured voltage and current. The energy is the time integral of this product.

The gas to be cleaned flows through the 3.5 m long stainless steel tube reactor, inner diameter 250 mm. The inside wall is smooth or can be fitted with needles. The center electrode is a conductive current at the cylinder, are prohibited to enter the EMC cabinet behind the integrator [7]. To avoid interference it is crucial that common mode currents do not enter the EMC cabinet behind the integrator [7]. The bandwidth of the DI systems used is 30 kHz–50 MHz. Passive integrators have been applied. Signal evaluation and corrections for the 50 \(\Omega\) load of the integrators were made as follows:

\[
V_X = k_3 V_{\text{out1}} + \alpha_1 \int k_1 V_{\text{out1}} \, dt
\]

and

\[
I_X = k_2 V_{\text{out2}} + \alpha_2 \int k_2 V_{\text{out2}} \, dt
\]

where \(V_{\text{out1}}\) and \(V_{\text{out2}}\) are the integrator outputs, \(k_3\) and \(k_2\) are the calibration factors, and \(\alpha_1\) and \(\alpha_2\) are the known correction factors for the integrator droop.

The E field at the cylinder electrode can be measured by means of a grid sensor, mounted flush with the surface of this electrode [11]. Fig. 4 shows the construction of this sensor.

1. **III. MEASURING SYSTEMS**

The base of the reactor vessel is a one-turn Rogowski coil (a toroid of rectangular minor cross section) to measure the external (corona) current \(I_e\). The central wire is fed into the reactor via a HV feedthrough, which also contains a capacitive sensor to form a differentiating-integrating (DI) measuring system for the external (corona) voltage \(V_e\) [9], [10]. In a DI system it is the strong differentiated signal that is transported via the coaxial cable to the passive RC input section of an integrator at the wall of an EMC cabinet. The integrator restores the original waveform but it also acts as an effective EMC filter. Large common mode currents are allowed to flow on the signal cables from sensor to integrator and back via grounding systems. A sufficiently low transfer impedance of these cables leaves the measured signal undisturbed. To avoid interference it is crucial that common mode currents do not enter the EMC cabinet behind the integrator [7]. The bandwidth of the DI systems used is 30 kHz–50 MHz. Passive integrators have been applied. Signal evaluation and corrections for the 50 \(\Omega\) load of the integrators were made as follows:

\[
V_X = k_3 V_{\text{out1}} + \alpha_1 \int k_1 V_{\text{out1}} \, dt
\]

and

\[
I_X = k_2 V_{\text{out2}} + \alpha_2 \int k_2 V_{\text{out2}} \, dt
\]

where \(V_{\text{out1}}\) and \(V_{\text{out2}}\) are the integrator outputs, \(k_3\) and \(k_2\) are the calibration factors, and \(\alpha_1\) and \(\alpha_2\) are the known correction factors for the integrator droop.

The E field at the cylinder electrode can be measured by means of a grid sensor, mounted flush with the surface of this electrode [11]. Fig. 4 shows the construction of this sensor.

It consists of a measuring electrode (a brass plate with a diameter of 30 mm) behind a grounded stainless steel grid (mesh size 1.4 mm). The distance between the plate and the grid is 2 mm. Charge carriers, which would normally produce a conductive current at the cylinder, are prohibited to enter the grid sensor by a repelling E field between the grounded grid and the plate, which is at a DC bias voltage of 15 V. This bias voltage and the voltage pulse at the central wire have the same polarity. Since the grid is not perfectly shielding, still some 2% of the corona E field is seen by the plate. This transient field produces a displacement current to the plate. The resulting signal is easily distinguished from the DC bias of the sensor. Related techniques to detect the E field are given by other authors [12], [13]. To obtain the total displacement current \(I_D\) to the cylinder electrode, the current to the plate of the E-field sensor needs to be multiplied by a factor that accounts for the ratios of surface area and grid penetration. Finally the current must be integrated in the time domain to obtain the displacement charge \(Q_D\), which is proportional to the E field at the cylinder. The bandwidth of this system is 0.5 Hz–50 MHz.

Operating as ion sensor, a forward DC-bias voltage (900 V) on the plate is applied to attract the ions into the grid sensor toward the plate. The resulting conduction current to the plate is a measure for the number of ions arriving at the sensor. The mesh size of the grid is small enough to strongly reduce the corona E field, as is necessary for the ion measurements.

For registrations of the voltage, current, and E-field signals a Nicolet 450 digital oscilloscope, 200 MSA/s, and an HP 54542 A digital oscilloscope, 2 GSa/s were used.

Chemical analysis was done with an HP 5880 gas chromatograph and a flame ionization detector (FID). For propane, butane, pentane, and ethylene a packed column porapak Q was used, for styrene, toluene, and 1,1,1-trichloro-ethane we used a packed SE 54 column. For styrene and toluene temperature programmed runs were made. The NO content of the flue gas of a gas-fueled engine at an industrial site was detected with a chemiluminescence method. All NO measurements in the laboratory were made with a testo 342-2 flue gas analyzer.

In the laboratory, the gas flow to be cleaned was composed by mixing contaminant with an airflow. This mix was fed to the main airflow, produced by pumping environmental air (1.5% \(\text{H}_2\text{O}\)) through the reactor [14]. Main airflow was measured with a testovent 4300 anemometer. Contaminants were fed in through Brooks mass flow controllers. In the case of styrene, toluene, pentane, and 1,1,1 trichloro-ethane, a heated bubbler was used for evaporation. The bubbler was followed by a cool down vessel (20°C) and the dry airflow into the bubbler was set with a mass flow controller; see Fig. 5. The flow from this system was added to the bulk flow of environmental air through the reactor. In and output concentrations to the reactor were determined from the known input flow and from subsequent measurements with the same instrument while the reactor was in the on or off state.
The total corona current, measured externally as $I_X$, can be represented [1] as a conductive component $I_C$ (passing charge carriers) plus a displacement component (changing E field) $I_D$. This component, measured separately with the E-field sensor, equals the current $I_0$ due to the changing external voltage $V_X$ across the vacuum capacitance $C_0$ between the electrodes, plus the current $I_S$ due to the movement of space charge in the gas

$$I_X = I_C + I_D = I_C + I_0 + I_S$$  \hspace{1cm} (3a)

and

$$I_0 = C_0 \frac{dV_X}{dt}$$  \hspace{1cm} (3b)

A number of CCD images (5 ns gating) are recorded in successive discharges to display the development of the corona discharge. The direction of view of the CCD camera was axial, parallel to the corona wire. CCD images cover the full cross section of the cylindrical reactor. From each recorded image we copy a strip running from wire to wall and combine these strips into one picture, a CCD movie, as shown in Fig. 6.

### IV. DISCHARGE DEVELOPMENT

Both positive and negative corona show similar behavior. First, many streamers develop from the wire toward the cylinder during the initial streamer phase [1]. The strongly inhomogeneous space charge at the streamer head creates a large E field, which causes an enhanced ionization and further growth of the initial streamers toward the cylinder. Each streamer carries a current of 0.1–1 A. The capacitance between the streamer head and the cylinder acts as a limiting impedance for the current through the initial streamer. The conductive streamer phase starts after the arrival of the initial streamers at the cylinder. The development of the initial streamer into a complete channel between the wire and the cylinder results in a disappearance of the capacitance between the streamer head and the cylinder. This allows a much larger current (1–10 A) to flow through each streamer; many streamers in parallel carry the large current of the pulsed corona discharge.

The curves for the measured charges $Q_X$ (total) and $Q_D$ (displacement only) are equal until the arrival of the initial streamers at the cylinder. After arrival a conductive current at the cylinder causes a separation of the curves $Q_X$ and $Q_D$. With a negative polarity at the wire, corona also develops at the needles covering the cylinder electrode. The resulting conductive current causes an early separation between the curves $Q_X$ and $Q_D$.

Based on current and voltage measurements a calculation was made of the energy input during the initial and the conductive streamer phase of a positive polarity discharge. The results are given in Fig. 7. It turns out that after the completion of a pulse, about one third of the corona energy is a result of the initial streamer phase and 2/3 results from the conductive streamer phase. If the indications are correct that the amount of corona energy is the important parameter for chemistry then the conductive streamer phase can add considerably to the conversion process.

### V. REACTOR MODEL

An exponential behavior for the VOC’s removal by the pulsed corona reactor was found experimentally and was given as [15]

$$X = 1 - \exp(-E/\Delta E)$$  \hspace{1cm} (4)

The dimensionless $X$ is the amount removed divided by the amount on input, where both amounts can be consistently expressed either in terms of $g/h$ or as concentration, e.g., mole fraction or parts per million. The parameter $E$ is the applied corona energy per unit volume and it will be shown now that $\Delta E$ is an apparent activation energy per unit volume for a mixture of a specific VOC plus air. Within the concentration ranges that we tested this apparent activation energy for the mixture is independent of the VOC’s concentration. An analysis based on gas dynamics and reaction kinetics is used to explain the exponential behavior and apparent activation energy. The reactions are activated by use of corona energy in an oxidating environment. Since the concentration of reactants formed in the environmental air by the corona discharge is high compared to the VOC’s concentration only first order reactions are considered. As the mechanism for the reaction is not known, an alternative expression for the rate constant $k$ [number of transitions per second] of the reaction will be needed.

With the experimental data we can find Peclet numbers of $10^4$–$10^5$ which means we are dealing with a plug flow reactor. In our tubular plug flow reactor we have Reynolds numbers of $2000$–$10^4$ which means that the flow is turbulent. With this knowledge we can make the following assumptions:

- only energy from the corona discharge is used for decomposition;
- the apparent activation energy is independent of the VOC’s concentration (ad hoc, verified by experiment);
- the reactor is an ideal plug flow reactor;
- only first order reactions are considered;
- an alternative expression for the rate constant $k$ is postulated.

A negative free energy change of a reaction means that after the reactions the products are at a lower free energy level. However, if bonds are broken, the reactants must go up an energy hill first, before they will go downhill. The activation of VOC’s plus air can be reached by using corona energy [14]. We are concerned about the apparent activation energy.
energy $\Delta E [J/l]$ needed for the decomposition of VOC’s in the mixture. For the rate constant $k$ [number of transitions per second] of the reaction we postulate a simple alternative expression [14]

\[ k = \frac{\gamma P}{\Delta E} \]  

(5)

where $P$ is the corona power per $m^3$ and $\gamma$ the used fraction of this power. The apparent activation energy per $m^3$, $\Delta E$, varies with the concentration of the mixture air plus VOC’s

\[ \Delta E = \Delta E_0 C_{\text{mix}}/C_{\text{mix0}}. \]  

(6)

Here $C_{\text{mix}}$ is number of moles of mixture per unit volume [mol/m$^3$] and $C_{\text{mix0}}$ and $\Delta E_0$ are the values at standard temperature and pressure (STP) conditions.

The reaction rate $R$ (number of moles converted per second per $m^3$) of a first order reaction is

\[ R = kC. \]  

(7)

The VOC’s concentration is $C$. The reaction rate is substituted in the continuity equation

\[ \frac{\partial C}{\partial t} + u \frac{\partial C}{\partial z} = -R \]  

(8)

for the flow in the reactor. The flow velocity is $u$ [m/s] in the direction along the axial $z$ coordinate of the cylinder.

To find the stationary solution of (8) we integrate along the length of the reactor and arrive at the desired exponential relation given above in (4).

The exponential relationship is very useful for fitting measured data in many cases. Some removal processes however do not fit the model.

**VI. CONVERSION OF VOC’s AND NO**

Simultaneous removal of NO and ethylene to obtain clean CO$_2$ from the exhaust of a power generating combustion
During generation of 110 kW of electrical power, the flue gas was treated by the pulsed corona pilot unit. The unit was running at a corona power level of up to 600 W. NO removal (oxidation into NO\(_2\)) was determined in terms of g/h (NO and total NO\(_x\) measurements were taken before the scrubber and before the reactor, nitric acid was not measured). Removal of other flue gas fractions such as ethylene was found to be minimal, most probably due to the large NO load of 1.6 kg/h. NO has the lowest apparent activation energy and is therefore processed more easily. Fig. 9 shows the resulting NO-removal rate as a function of corona power. Since a relatively small fraction of the high NO load was removed, we see a high removal efficiency (95 g/kWh). It is clear that we are in the initial part of the exponential function \(X(E)\) given in (4).

In the laboratory it was clearly shown that styrene, toluene, ethylene, and NO-ethylene mixtures can be decomposed to a high degree with our pulsed corona reactor. The VOC’s propane, butane, pentane, and 1,1,1 trichloro-ethane are not completely decomposed. Table I gives an overview of chemical measurements. We now compare the calculated conversion using (4) and the measured conversion. It is found that the model fits in the cases of: styrene, toluene, 1,1,1 trichloro-ethane, ethylene, NO, and pentane. The conversion for propane and butane calculated with (4) does not fit the experimental data. Part of this conversion may require additional intermediate products which is not in line with the assumption of a first order reaction. Fitted values for \(\Delta E_0\) are summarized in Table I. The fit for toluene is illustrated in Fig. 10 by a graph of measured values \(X_{\text{measured}}\) (amount removed divided by amount on input both taken from toluene measurements) versus calculated values for the conversion, \(X_{\text{model}}\) (amount removed divided by amount on input as calculated from (4) by using the measured corona energy density and the fitted value for the apparent activation energy). Here the full range of residence times, concentrations, and corona energies is covered by (4) and a single value for \(\Delta E_0\).

Apparent activation energies found in this work are compared with \(\Delta E_0\) values derived from results of other researchers [16]–[22]. A summary can be found in Table II.
TABLE I
OVERVIEW OF CHEMICAL MEASUREMENTS AND DECOMPOSITION OF VOC’s IN AIR. THE VALUES FOR THE APPARENT ACTIVATION ENERGY $\Delta E_0$ ARE FITTED ACCORDING TO (4) AND (6)

<table>
<thead>
<tr>
<th>Substance</th>
<th>$M$ [kg/kmol]</th>
<th>Concentration [ppm]</th>
<th>Mass flow [g/h]</th>
<th>Corona Power [kW]</th>
<th>Corona energy kWh per kg load to reach 63% removal</th>
<th>$\Delta E_0$ [J/liter]</th>
</tr>
</thead>
<tbody>
<tr>
<td>NO</td>
<td>30</td>
<td>213</td>
<td>6.5-23</td>
<td>0.15 - 1.10</td>
<td>15</td>
<td>16.5</td>
</tr>
<tr>
<td>Toluene</td>
<td>92</td>
<td>125 - 450</td>
<td>18-40</td>
<td>0.13 - 1.16</td>
<td>24</td>
<td>98.8</td>
</tr>
<tr>
<td>Styrene</td>
<td>104</td>
<td>30 - 190</td>
<td>15-87</td>
<td>0.25 - 2.54</td>
<td>7</td>
<td>11.3</td>
</tr>
<tr>
<td>1,1,1 TCA</td>
<td>133</td>
<td>80 - 1000</td>
<td>4-25</td>
<td>0.13 - 1.13</td>
<td>180</td>
<td>135</td>
</tr>
<tr>
<td>Pentane</td>
<td>72</td>
<td>80 - 1000</td>
<td>6-73</td>
<td>0.14 - 1.04</td>
<td>88</td>
<td>185</td>
</tr>
<tr>
<td>Ethylene</td>
<td>28</td>
<td>150 - 2500</td>
<td>17-114</td>
<td>0.16 - 1.23</td>
<td>12</td>
<td>41.2</td>
</tr>
<tr>
<td>Propane</td>
<td>44</td>
<td>10 - 500</td>
<td>1.7-36</td>
<td>0.16 - 1.15</td>
<td>180</td>
<td>-</td>
</tr>
<tr>
<td>Butane</td>
<td>58</td>
<td>50 - 2000</td>
<td>9-111</td>
<td>0.14 - 1.19</td>
<td>75</td>
<td>-</td>
</tr>
</tbody>
</table>

Fig. 10. Measured conversion of toluene versus calculated conversion using the model represented by (4). The full range of flow rates, input concentrations, and applied corona power is covered.

VII. EFFICIENCY

The transport of energy from mains AC power to chemical processes can be divided in three separate conversion steps [23].

1) Energy from mains power into high-voltage pulses.
2) High-voltage energy into corona discharge energy in the gas.
3) Corona energy finally used for chemical processes.

The NO removal process was chosen for investigation of the efficiencies of the three separate steps of energy transport. At the same time we investigated the effect of polarity on these efficiencies. An overview of the results is given in Fig. 11.

The conversion in steps 1) and 2) was determined from the electrical measurements on mains power and on corona power.

The application of corona energy for chemical processes, step 3), was expressed as amount of substance processes per kWh of the corona energy from step 2). Step 3) is found to be independent of polarity, i.e., chemistry is polarity independent here.

Step 2) energy transfer, however, is very much affected by polarity choice. A positive wire gives a better energy transfer when polarity effects are compared at the same external voltage. As we know from previous work [1], a negative wire

TABLE II
APPEARENT ACTIVATION ENERGIES $\Delta E_0$ [J/liter] FROM THIS WORK AND FROM THE WORK BY ROUSH ET AL. [21], COMPARED WITH DATA DERIVED FROM THE WORK OF PENTRANZE ET AL. [16]-[20] AND THE WORK OF COOGAN ET AL. [22]. REMOVAL IS $X = 1 - \exp(-E/\Delta E)$, WHERE $E$ IS THE APPLIED CORONA ENERGY PER UNIT VOLUME

<table>
<thead>
<tr>
<th></th>
<th></th>
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<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>NO</td>
<td>16.5</td>
<td>50</td>
<td>10</td>
<td>10-21</td>
<td></td>
</tr>
<tr>
<td>Toluene</td>
<td>98.8</td>
<td>120</td>
<td>91-253</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Styrene</td>
<td>11.3</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>C Cl₄</td>
<td></td>
<td>219</td>
<td>44</td>
<td></td>
<td></td>
</tr>
<tr>
<td>TCA (1,1,1)</td>
<td></td>
<td>555</td>
<td>9</td>
<td></td>
<td></td>
</tr>
<tr>
<td>TCE</td>
<td>80</td>
<td>16</td>
<td>9</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Benzene</td>
<td></td>
<td>500</td>
<td>39</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Pentane</td>
<td></td>
<td>185</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Ethylene</td>
<td></td>
<td>41.2</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Propane</td>
<td></td>
<td>do not fit model</td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Butane</td>
<td></td>
<td></td>
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</tr>
</tbody>
</table>

Remarks:
- LANL in N₂, 20 % O₂, 1% H₂O
- LLNL normal in N₂
- Italics: in dry air
- Roush-Hutherson values depending on pulse parameters
needs a higher voltage to produce intense coronas. This effect is not accounted for in this study, we applied the same voltage level for both polarities.

VIII. CONCLUSIONS

Simultaneous recordings with CCD camera and electrical diagnostics allow a clear analysis of the high intensity corona development. Initial streamer phase and transition to a conductive streamer phase are detected and an excellent correlation is found between all data from electrical records and CCD movies. The energy input during the various streamer developments was followed.

Chemical conversion processes initiated by the pulsed corona were tested in the lab but also at industrial locations. A model that only needs two parameters, apparent activation energy and corona energy, can in many cases explain the correlation is found between all data from electrical records and CCD movies. The energy input during the various streamer developments was followed.

With respect to pulsed power, reliability can be further increased from the established 350 h of continuous operation to considerably longer times.

The EMC of pulsed power for pollution control can be designed to perform perfectly. Following a well-defined approach, pulsed power was constructed such that no interference at all occurred with surrounding and internal equipment.

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REFERENCES


Since 1995, he has been employed on the Pulsed Corona Pilot Project of the High-Voltage and EMC group of the EUT. His interests are high-voltage techniques, EMC, pulsed power, and the influence of electrical energy on chemical processes.

Bert E. J. M. van Heesch was born in 1951 in Utrecht, The Netherlands. He received the master’s degree in physics in 1975 and the Ph.D. degree in plasma physics and fusion related research in 1982.

He has been leading Eindhoven corona and pulsed power research since 1986. Prior, he was occupied with fusion technology in Jutphaas, The Netherlands, in Suchumi, Russia, and Saskatoon, Canada. Among his designs are a toroidal fusion experiment (5 GW pulse power), a particle beam diagnostic, a substation high-voltage measuring system, and a unit for continuous pulsed power corona.

Sander S. V. B. van Paasen was born in Ysselstein, The Netherlands, in 1972. He received the degree in chemical engineering from the Eindhoven Polytech, The Netherlands, in 1993, and the M.Sc. degree in chemical engineering from Eindhoven University of Technology in 1996.

After his degree he joined the Process Technology Group and High-Voltage and EMC Group at the Eindhoven University to participate in the pulsed corona project for gas treatment. Since 1997 he has worked as a process and product designer in trainee-ship at the University.

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