ESR studies on hydrodesulfurization catalysts: nickel- or cobalt-promoted sulfided tungsten- or molybdenum-containing catalysts

Citation for published version (APA):

DOI:
10.1016/0021-9517(81)90268-2
10.1016/0021-9517(81)90268-2

Document status and date:
Published: 01/01/1981

Document version:
Publisher's PDF, also known as Version of Record (includes final page, issue and volume numbers)

Please check the document version of this publication:
• A submitted manuscript is the version of the article upon submission and before peer-review. There can be important differences between the submitted version and the official published version of record. People interested in the research are advised to contact the author for the final version of the publication, or visit the DOI to the publisher's website.
• The final author version and the galley proof are versions of the publication after peer review.
• The final published version features the final layout of the paper including the volume, issue and page numbers.

Link to publication

General rights
Copyright and moral rights for the publications made accessible in the public portal are retained by the authors and/or other copyright owners and it is a condition of accessing publications that users recognise and abide by the legal requirements associated with these rights.

• Users may download and print one copy of any publication from the public portal for the purpose of private study or research.
• You may not further distribute the material or use it for any profit-making activity or commercial gain
• You may freely distribute the URL identifying the publication in the public portal.

If the publication is distributed under the terms of Article 25fa of the Dutch Copyright Act, indicated by the "Taverne" license above, please follow below link for the End User Agreement:
www.tue.nl/taverne

Take down policy
If you believe that this document breaches copyright please contact us at:
openaccess@tue.nl
providing details and we will investigate your claim.

Download date: 28. Dec. 2019
ESR Studies on Hydrodesulfurization Catalysts: Nickel- or Cobalt-Promoted Sulfided Tungsten- or Molybdenum-Containing Catalysts

A. J. A. Konings, W. L. J. Brentjens, D. C. Koningsberger, and V. H. J. de Beer

Laboratory for Inorganic Chemistry, Eindhoven University of Technology, P.O. Box 513, 5600 MB Eindhoven, The Netherlands

Received March 5, 1980; revised July 15, 1980

ESR spectra of nickel- or cobalt-promoted sulfided tungsten- or molybdenum-containing catalysts are measured together with the influence of equilibration at different H₂S/H₂ ratios and CO adsorption hereon. The ESR measurements are compared with thiophene hydrodesulfurization (HDS) activities. The influence of nickel and cobalt on the ESR spectra is essentially the same. This similarity also holds for the thiophene HDS activities. A new signal VI (g = 2.06, ΔH = 220 G for Ni-Mo; g = 2.08, ΔH = 220 G for Ni-W) not occurring in unpromoted catalysts is detected. The intensities of signals II, III, IV, and VI are dependent on the composition of the interacting atmosphere. The results are discussed in terms of W₈(S₈)₆(W₈S₈)₆ crystallite edge decoration with promotor ions. Possible surface configurations corresponding with the different paramagnetic sites are described.

INTRODUCTION

It is widely accepted by now that the catalytic active phase of the intensively applied hydrodesulfurization catalyst systems consists of MoS₂(WS₂) crystallites (1, 2). The catalytic activity can be enhanced (promoted) by nickel or cobalt, often referred to as promoter ions. It is the role of these promoter ions that is still not well understood. Several models have been proposed. The basic idea of the intercalation model (pseudointercalation or decoration seems to describe the proposed interaction better) from Farragher and Cossee (3) is the incorporation of promotor ions in octahedral holes between the MS₈ layers, restricted to the crystal edges. The reorganization of the surface due to this incorporation should lead to an increase of active sites. The model based on synergy by contact proposed by Delmon and co-workers (4) describes the promotor action as an electron transfer between surfaces of MoS₂(WS₂) and Co₉S₈(Ni₅S₈) crystallites.

Surface W³⁺(Mo³⁺) ions connected with anion vacancies play the role of the catalytic active centers in the decoration model. Since W³⁺ ions are paramagnetic, ESR can be used to study the active centers. The ESR results obtained at our laboratory for the unpromoted tungsten- or molybdenum-containing catalysts have been reported earlier (5). The necessity of measuring sulfided catalysts in situ has been demonstrated (5, 6). Five different signals could be analyzed in the ESR spectra of these catalysts. Signal I (oxo-Mo⁵⁺, g = 1.933, and oxo-W⁵⁺, g = 1.78) and possibly signal III arise as a result of interactions with the support. Three other signals originate from the disulfide phase. Signal II (g = 1.985 for Mo and g = 1.91 for W) and signal IV (g = 2.01 for W) show a complementary behavior upon evacuation and H₂S adsorption and are therefore ascribed to paramagnetic surface species. It has been attempted to assign signals II and IV to surface M³⁺ or M⁵⁺ ions with different sulfur ligand symmetries. The origin of another signal (V) remained unexplained but it might be re-
lated with the presence of bulk defect structures.

In the present study the influence of the promotor ions upon the paramagnetic species mentioned above will be demonstrated for the systems Ni(Co)–W(Mo)/SiO₂(γ–Al₂O₃). Spectra of cobalt-promoted alumina-supported catalysts are not shown since the signal originating from Co²⁺ ions in the support interferes with the signals from the disulfide phase. For a few tungsten-containing catalysts the effect of variations in the H₂S/H₂ ratio (equilibration) as well as carbon monoxide adsorption will be demonstrated.

The system Ni–W has been studied earlier by Voorhoeve (7). He reported a correlation between benzene hydrogenation activity and intensity of an ESR signal most probably identical to our signal IV (5). Probably due to catalyst pretreatment (sulfidation procedure) the intensities of signals II and V are low in his samples.

The drastic change in g-value and the decrease in number of paramagnetic species upon introduction of promotor ions found in the present study will be discussed in terms of surface reorganization caused by these promotor ions.

EXPERIMENTAL

Catalyst Preparation

All starting materials were free from interfering paramagnetic impurities.

Silica-supported catalysts. SiO₂ (Ketjen F-2) was successively washed with excess ammonia (4.5 N) and distilled water. After drying at 383 K for 16 hr it was calcined in air at 873 K for 16 hr. The pore volume was then 1.05 cm³ g⁻¹ and the surface area 400 m² g⁻¹. Aqueous solutions of analytical-grade ammonium heptamolybdate (Merck), ammonium metatungstate (Koch–Light Laboratories Ltd.), nickel nitrate (BDH), or cobalt nitrate (Merck) were used for pore volume impregnation. Silica was first impregnated with ammonium heptamolybdate or ammonium metatungstate, dried 16 hr at 383 K, calcined in air 16 hr at 773 K, and sulfided under standard conditions described below.

Then nickel or cobalt was introduced, followed by drying for 16 hr at 383 K and the standard sulfiding procedure. This “double” sulfiding was used for silica-supported samples to prevent the formation of cobalt or nickel molybdates or tungstates (8).

Alumina-supported catalysts. γ-Al₂O₃ was prepared by calcining boehmite (Martinwerk GmbH) in air for 2 hr at 873 K. The pore volume was then 0.35 cm³ g⁻¹ and the surface area 215 m² g⁻¹. The same aqueous solutions as mentioned above were used for pore volume impregnation. First alumina was impregnated with ammonium heptamolybdate or ammonium metatungstate, dried 16 hr at 383 K, calcined in air at 773 K, then nickel nitrate solution was added, followed by drying 16 hr at 383 K, and calcining 16 hr at 773 K in air. Finally the catalyst was sulfided under standard conditions.

Sulfiding Procedure

Catalysts samples (200 mg) were treated in H₂ containing 16% (v/v) H₂S at a flow rate of 50 cm³ min⁻¹ and using the following temperature program: 10 min 295 K, linear increase from 295 to 673 K in 260 min, 20 hr 673 K, quenching to 295 K. It has been demonstrated (5, 6) that the properties of sulfided catalysts change upon exposure to oxygen. We therefore used a special ESR reactor to prevent contamination of the sample by oxygen (5). Hydrogen was deoxygenated over BTS catalyst (BASF R3-11) and dried over molecular sieves (Union Carbide 4A). Hydrogen sulfide (Matheson CP grade) was used as supplied.

Equilibration Procedure

Tungsten and nickel–tungsten-containing catalysts were treated with hydrogen containing 1 or 0.01% (v/v) H₂S, at 673 K for 24 hr, immediately after the standard sulfiding procedure was completed. These
samples were then quenched to 295 K and measured under the H₂S/H₂ atmosphere as used for equilibration. The H₂S/H₂ gas mixtures (Air Liquide) containing H₂S of 99% and H₂ of 99.9999% purity were used without further purification. The composition of these gas mixtures was checked frequently during each equilibration experiment.

**Carbon Monoxide Adsorption**

Freshly sulfided W(19.3)/SiO₂ and Ni(4)-W(19.3)/SiO₂ samples (numbers in parentheses are wt% NiO and WO₃, respectively) were evacuated (<10⁻¹ Torr, 295 K) and contacted with 40 Torr CO (10 min at 295 K and 15 min at 473 K). ESR spectra were recorded after each treatment (sulfiding, evacuation, CO at 295 K, and CO at 473 K). Carbon monoxide (Matheson CP grade) was used as supplied.

**ESR Measurements**

The ESR measurements were carried out using a Varian E-15 spectrometer equipped with a TE 104 dual-sample cavity. A Varian Strong Pitch sample (g = 2.0028, 3 × 10¹⁵ spins cm⁻¹) was used to calibrate the magnetic field, and functioned as a standard for the quality factor of the ESR cavity. Accuracy of the calculated relative and absolute signal intensities was 10 and 25%, respectively. In order to determine signal intensities as accurately as possible, ESR spectra were recorded in the temperature range 20–100 K (in a few cases 4–300 K) by means of a liquid-helium continuous-flow cryostat (Oxford Instruments).

**HDS Activity Measurements**

Thiophene conversion measurements were performed at atmospheric pressure and 673 K in a continuous flow reactor (9). Catalyst (200 mg) was presulfided with H₂ containing 16% (v/v) H₂S at a flow rate of 50 cm³ min⁻¹, using the following temperature program: 10 min 295 K, linear temperature increase from 295 to 673 K in 1 hr, 2 hr 673 K. Then the gas mixture was changed to H₂ with 7% (v/v) thiophene, 50 cm³ min⁻¹. Thiophene HDS and butene hydrogenation data were obtained with stabilized (2-hr run) catalysts. Although the sulfiding procedure differs from the one used to prepare samples for ESR measurements it is believed that the obtained activities are at least indicative for their sequence to one another.

**RESULTS**

The various ESR signals that we have detected in sulfided catalysts are displayed in Figs. 1–6 (measured at 20 K). They are indicated by arrows at the approximate position of their low-field peaks which are found to be better resolved than the high-field peaks (5). Only those low-field peaks which are clearly observable are indicated. Since the signals show considerable overlap, it is difficult to determine the ESR parameters of each signal accurately. The g-value and linewidth for those signals that could be detected separately, are tabulated in Table 1. In Table 2 we have indicated which signals are present or absent in each sample, together with the total number of spins (TNS) from the signals in the disulfide phase.

**Influence of Promotor Ions**

In Fig. 1 the spectra of standard sulfided Mo(12)/SiO₂, Ni(0.4)–Mo(12)/SiO₂, Ni(4)–Mo(12)/SiO₂, Mo(12)/γ-Al₂O₃, and Ni(4)–Mo(12)/γ-Al₂O₃ are shown. Two signals (II and V) are observable in the spectrum of Mo(12)/SiO₂ (Fig. 1a). It has been shown earlier (5) that signals II and V originate from two different paramagnetic sites. Introduction of a small amount of nickel, Ni(0.4) Mo(12)/SiO₂ (Fig. 1b), leads to an intensity decrease of signal II and a broadening of the left-hand wing of the spectrum. A tenfold increase of the nickel content, Ni(4)–Mo(12)/SiO₂ (Fig. 1c), causes signal II to decrease further. The left hand wing of the spectrum increases more, possibly caused by the generation of a new signal
(VI). Signal V decreases now in intensity. Signal I (oxo-Mo⁵⁺) (5) reappears and a signal at \( g = 1.96 \) shows up.

A comparison of the ESR spectra of standard sulfided Mo(12)/\( \gamma \)-Al₂O₃ (Fig. 1e) and Ni(4)-Mo(12)/\( \gamma \)-Al₂O₃ (Fig. 1d) clearly shows that signal VI (\( g = 2.06, \Delta H = 220 \) G) is indeed a new signal. Signal II disappears completely and only a trace of signal V remains after introduction of nickel.

The silica-supported molybdenum samples show a higher intensity of signal V than alumina-supported molybdenum catalysts. The TNS hardly changes upon the introduction of promotor ions and is almost independent of the support material.

### TABLE 1

**ESR Parameters of the Signals**

<table>
<thead>
<tr>
<th>Signal</th>
<th>Molybdenum</th>
<th>Tungsten</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Compound</td>
<td>( g )</td>
</tr>
<tr>
<td>I</td>
<td>Mo(12)/( \gamma )-Al₂O₃</td>
<td>1.933</td>
</tr>
<tr>
<td>II</td>
<td>Mo(12)/SiO₂</td>
<td>1.985</td>
</tr>
<tr>
<td>III</td>
<td>Mo(12)/( \gamma )-Al₂O₃</td>
<td>1.965</td>
</tr>
<tr>
<td>IV</td>
<td>Ni(4)-Mo(12)/( \gamma )-Al₂O₃</td>
<td>2.06</td>
</tr>
<tr>
<td>VI</td>
<td>Ni(4)-Mo(12)/( \gamma )-Al₂O₃</td>
<td>2.06</td>
</tr>
</tbody>
</table>

**TABLE 2**

<table>
<thead>
<tr>
<th>Sample</th>
<th>Total number of spins (( \times 10^{18} )) g⁻¹</th>
<th>Signals</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>I</td>
<td>II</td>
</tr>
<tr>
<td>Mo(12)/SiO₂</td>
<td>5.4</td>
<td>VW</td>
</tr>
<tr>
<td>Mo(12)/( \gamma )-Al₂O₃</td>
<td>4.4</td>
<td>S</td>
</tr>
<tr>
<td>Ni(0.4)-Mo(12)/SiO₂</td>
<td>3.5</td>
<td>VW</td>
</tr>
<tr>
<td>Co(0.4)-Mo(12)/SiO₂</td>
<td>2.8</td>
<td>VW</td>
</tr>
<tr>
<td>Ni(4)-Mo(12)/SiO₂</td>
<td>3.5</td>
<td>S</td>
</tr>
<tr>
<td>Co(4)-Mo(12)/SiO₂</td>
<td>3.5</td>
<td>S</td>
</tr>
<tr>
<td>Ni(4)-Mo(12)/( \gamma )-Al₂O₃</td>
<td>4.5</td>
<td>S</td>
</tr>
<tr>
<td>W(19.3)/SiO₂</td>
<td>0.8</td>
<td>–</td>
</tr>
<tr>
<td>W(19.3)/( \gamma )-Al₂O₃</td>
<td>2.9</td>
<td>–</td>
</tr>
<tr>
<td>Ni(0.4)-W(19.3)/SiO₂</td>
<td>0.7</td>
<td>–</td>
</tr>
<tr>
<td>Co(0.4)-W(19.3)/SiO₂</td>
<td>0.8</td>
<td>–</td>
</tr>
<tr>
<td>Ni(0.4)-W(19.3)/( \gamma )-Al₂O₃</td>
<td>2.6</td>
<td>–</td>
</tr>
<tr>
<td>Ni(4)-W(19.3)/SiO₂</td>
<td>0.5</td>
<td>–</td>
</tr>
<tr>
<td>Co(4)-W(19.3)/SiO₂</td>
<td>0.7</td>
<td>–</td>
</tr>
<tr>
<td>Ni(4)-W(19.3)/( \gamma )-Al₂O₃</td>
<td>3.5</td>
<td>–</td>
</tr>
</tbody>
</table>

*a Numbers in parentheses are wt% MoO₃, WO₂, CoO, and NiO, respectively. All samples are sulfided under standard conditions; for details see Experimental section.

b Accuracy ±25%.

c = absent; VW = very weak; W = weak; S = strong; VS = very strong.
ESR STUDIES ON HYDRODESULFURIZATION CATALYSTS

FIG. 1. ESR spectra (recorded at 20 K): (a) Mo(12)/SiO₂, receiver gain (RG) 10⁵; (b) Ni(0.4)-Mo(12)/SiO₂, RG 2 x 10⁵; (c) Ni(4)-Mo(12)/SiO₂, RG 5 x 10⁵; (d) Ni(4)-Mo(12)/γ-Al₂O₃, RG 5 x 10⁵; (e) Mo(12)/γ-Al₂O₃, RG 10⁶. All samples are standard sulfided, for details see Experimental section. Numbers in parentheses are wt% NiO and MoO₃, respectively.

Fig. 2. ESR spectra (recorded at 20 K): (a) W(19.3)/SiO₂, RG 5 x 10⁵; (b) Co(0.4)-W(19.3)/SiO₂, RG 4 x 10⁵; (c) Ni(0.4)-W(19.3)/SiO₂, RG 4 x 10⁵; (d) Ni(4)-W(19.3)/SiO₂, RG 4 x 10⁵; (e) Co(4)-W(19.3)/SiO₂, RG 8 x 10⁵. All samples are standard sulfided. Numbers in parentheses are wt% NiO, CoO, and WO₃, respectively.

The influence of promotor ions on supported sulfided tungsten-containing catalysts is essentially the same as for the molybdenum system. The influence of nickel and cobalt on silica-supported samples is shown in Fig. 2. Increasing the promotor content from 0.4 wt% (Figs. 2b and c) to 4 wt% (Figs. 2d and e) results in a complete disappearance of signal II and a decrease of signal V. Nickel is more effective than cobalt in the breakdown of signal II.

The linewidth of signal VI is larger for cobalt-promoted Mo(12)/SiO₂ catalysts than the same observations were made.

The influence of promotor ions on supported sulfided tungsten-containing catalysts is essentially the same as for the molybdenum system. The influence of nickel and cobalt on silica-supported samples is shown in Fig. 2. Increasing the promotor content from 0.4 wt% (Figs. 2b and c) to 4 wt% (Figs. 2d and e) results in a complete disappearance of signal II and a decrease of signal V. Nickel is more effective than cobalt in the breakdown of signal II.

The linewidth of signal VI is larger for cobalt-promoted catalysts. The g-value and linewidth of signal VI are given in Table 1. Comparison of Figs. 2 and 3 (γ-Al₂O₃-supported catalysts) shows that the influence of the promotor (nickel) on the ESR signals of the tungsten system is independent of the support material.

There is, however, a big difference in the TNS between silica- and alumina-supported tungsten-containing catalysts, in contrast to the molybdenum-containing catalysts (see Table 2). The TNS for alumina-supported catalysts is about 5 times larger than that of the silica-supported samples and of the same order of magnitude as for the molybdenum system. The promotor ions have no influence on the TNS.

The tungsten system shows a considerable overlap of signal VI with signal V. The breakdown of signal II is more drastic in the tungsten system than in the molybdenum system.
catalysts. Signal I (oxo-W\(^{3+}\)) (5) does not appear in the spectra of tungsten catalysts after introduction of promotor ions.

**Effects of Equilibration**

In Figs. 4 and 5 the spectra of equilibrated alumina-supported tungsten- and nickel–tungsten-containing catalysts are presented. From Figs. 4a, b, and c (W(19.3)/\(\gamma\)-Al\(_2\)O\(_3\) equilibrated at \(\text{H}_2\text{S}/\text{H}_2 = 0.16\), \(10^{-2}\), and \(10^{-4}\), respectively) it appears that the intensity of signal II decreases with decreasing \(\text{H}_2\text{S}/\text{H}_2\) ratio. In spectrum 4c a signal (III, \(g = 1.98\), \(\Delta H = 40\) G) is observable which is the equivalent of signal III detected earlier (5) in Mo(12)/\(\gamma\)-Al\(_2\)O\(_3\) after treatment of a standard sulfided sample with 7% (v/v) thiophene in helium at 423 K. This signal has not been detected before in the tungsten system. The TNS and the intensity of signal V hardly change after equilibration. For W(19.3)/SiO\(_2\) the same effects are observed.

In Figs. 4d and e the spectra of Ni(0.4)–W(19.3)/\(\gamma\)-Al\(_2\)O\(_3\) (calcined at 1073 K), standard sulfided and equilibrated at \(\text{H}_2\text{S}/\text{H}_2 = 10^{-4}\), respectively, are given. The effects of equilibration are the same as for the unpromoted catalyst: signal II decreases in intensity and signal III shows up. The \(g\)-value resulting from the sum of signals V and VI shifts to a higher value. There is a strong oxo-W\(^{3+}\) signal (I) present in these samples due to the high calcination temperature (1073 K, 16 hr).

In Fig. 5 the spectra of equilibrated Ni(4)–W(19.3)/\(\gamma\)-Al\(_2\)O\(_3\) are shown. Only
200G - 2

FIG. 5. ESR spectra (recorded at 20 K) of Ni(4)-W(19.3)/γ-Al₂O₃: (a) standard sulfided, RG 5 × 10⁶; (b) equilibrated at 673 K, H₂S/H₂ = 10⁻⁴, RG 5 × 10⁶; (c) equilibrated at 673 K, H₂S/H₂ = 10⁻¹, RG 10⁶; (d) equilibrated at 613 K, H₂S/H₂ = 10⁻⁴, RG 5 × 10⁶.

signals V and VI from the disulfide phase are present. Lowering the H₂S/H₂ ratio leads to a shift of the g-value to a higher value and also the left-hand top of the spectrum shifts to the left (Figs. 5c and d). Signal V seems to diminish and signal VI is converted into a signal with slightly different parameters. Figure 5c, Ni(4)-W(19.3)/γ-Al₂O₃ equilibrated at 673 K with H₂S/H₂ = 10⁻⁴, shows a very broad underlying signal which does not appear in the corresponding Ni(0.4)-W(19.3)/γ-Al₂O₃ sample (Fig. 4c) nor in the sample where the equilibration temperature was 613 K (Fig. 5d). The TNS for this catalyst is hardly affected by equilibration.

Effects of CO Adsorption

The vacuum treatment at 295 K did not influence the ESR spectra of W(19.3)/SiO₂ or Ni(4)-W(19.3)/SiO₂. The effect of subsequent CO adsorption at 295 and 473 K is shown in Fig. 6. CO adsorbed on W(19.3)/SiO₂ at 295 K results only in a slight intensity decrease of signal II (Fig. 6b). When CO was adsorbed at 473 K signal II disappeared and a twofold intensity increase of signal IV (ESR parameters after CO adsorption: g = 2.00, ΔH = 80 G) was observed (Fig. 6c). Signal IV was detected earlier (5) in bulk WS₂ (g = 2.01 and ΔH = 180 G, values difficult to determine). Subtraction of spectrum 6b from 6c clearly shows that signal IV is the increasing signal.

For Ni(4)-W(19.3)/SiO₂, CO adsorption at 295 K (Fig. 6e) already gives an increase in signal intensity. The parameters of the
signal are slightly different from signal VI 
\((g = 2.060, \Delta H = 180 \text{ G})\). When CO is 
adsorbed at 473 K a sixfold increase of the 
signal intensity is observed (Fig. 6f). In all 
cases it is difficult to estimate the contribu-
tion of signal V to the signal intensity.

**Temperature Dependence of the Signal Intensity**

In Fig. 7 the reciprocal signal intensity 
(double integration of the spectrum without 
signal I) versus the temperature is plotted 
for standard sulfided W(19.3)/SiO\(_2\) and 
Ni(4)–W(19.3)/SiO\(_2\). The temperature re-

gion for which the Curie–Weiss law holds is 
20–200 K for W(19.3)/SiO\(_2\) and 20–100 K 
for Ni(4)–W(19.3)/SiO\(_2\). Molybdenum- 
containing catalysts show the same behavior. 
In this region the TNS has been calculated.

**Activity Measurements**

Thiophene HDS and butene hydrogenation 
activity data are listed in Table 3. The 
reaction rate for thiophene HDS has been 
calculated on the basis of a pseudo-first- 
order reaction in thiophene. The hydroge-
nation to butane of the butenes formed 
upon HDS, is expressed as percentage but-
ane over butenes + butane (insufficient 
data for reaction rate determination).

![Fig. 7. Temperature dependence of the signal (II–VI) intensity. (a) Ni(4)–W(19.3)/SiO\(_2\); (b) W(19.3)/SiO\(_2\). Standard sulfided samples.](image)

**TABLE 3**

<table>
<thead>
<tr>
<th>Sample</th>
<th>(r^b \times 10^9) HDS</th>
<th>Hydrogenation to butane (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Mo(12)/SiO(_2)</td>
<td>8.9</td>
<td>16</td>
</tr>
<tr>
<td>Mo(12)/γ-Al(_2)O(_3)</td>
<td>8.4</td>
<td>19</td>
</tr>
<tr>
<td>Ni(4)–Mo(12)/SiO(_2)</td>
<td>35.9</td>
<td>8</td>
</tr>
<tr>
<td>Co(4)–Mo(12)/SiO(_2)</td>
<td>29.4</td>
<td>8</td>
</tr>
<tr>
<td>Ni(4)–Mo(12)/γ-Al(_2)O(_3)</td>
<td>30.3</td>
<td>25</td>
</tr>
<tr>
<td>W(19.3)/SiO(_2)</td>
<td>3.8</td>
<td>7</td>
</tr>
<tr>
<td>W(19.3)/γ-Al(_2)O(_3)</td>
<td>2.8</td>
<td>9</td>
</tr>
<tr>
<td>Ni(0.4)–W(19.3)/SiO(_2)</td>
<td>18.0</td>
<td>7</td>
</tr>
<tr>
<td>Ni(0.4)–W(19.3)/γ-Al(_2)O(_3)</td>
<td>3.3</td>
<td>12</td>
</tr>
<tr>
<td>Ni(4)–W(19.3)/SiO(_2)</td>
<td>25.3</td>
<td>6</td>
</tr>
<tr>
<td>Ni(4)–W(19.3)/γ-Al(_2)O(_3)</td>
<td>28.6</td>
<td>12</td>
</tr>
</tbody>
</table>

* For test conditions see Experimental section.

\(\text{a}\) \(r = -(F/W) \ln(1 - x) = -0.045 \ln(1 - x)\).

The thiophene HDS activity is enhanced 
by a factor of 3–10 as a result of the addition 
of promotor ions. For tungsten-containing 
catalysts the promoting effect is more pro-
ounced than for the molybdenum system. 
The technique of “double” sulfiding makes it 
possible to prepare silica-supported cata-
ysts with HDS activities comparable with 
alumina-supported catalysts. The catalytic 
activity of alumina-supported catalysts is 
not enhanced by addition of a small amount 
of promotor (W(19.3)/γ-Al\(_2\)O\(_3\), \(r = 2.8 \times 10^{-3}\); Ni(0.4)–W(19.3)/γ-Al\(_2\)O\(_3\), \(r = 3.3 \times 10^{-3}\)) whereas the corresponding silica-sup-
ported catalysts show a fivefold increase of 
activity (W(19.3)/SiO\(_2\), \(r = 3.8 \times 10^{-3}\); Ni(0.4)–W(19.3)/SiO\(_2\), \(r = 18 \times 10^{-3}\)).

Although no reaction rate could be deter-
mined for the hydrogenation to butane it 
appears that for catalysts without promotor 
the hydrogenation activity is independent 
of the support. The alumina-supported pro-
moted catalysts show a two- to threefold-
higher hydrogenation activity than the silica-supported samples.

**DISCUSSION**

**Influence of Promotor Ions on the ESR Spectra**

Let us first summarize the results of the 
previous section. Introduction of a small
amount of promotor \((\text{Ni(Co)}/W(\text{Mo}) = 0.064 \text{ atomic ratio})\) causes a decrease of signals II, III, and V but they are still present or can be generated by a proper treatment (low \(\text{H}_2\text{S}/\text{H}_2\) ratio \(\rightarrow\) signal III). Signal IV seems to disappear completely and cannot be generated by equilibration or evacuation. (In unpromoted catalysts the intensity of signal IV increased after evacuation of the sample at 673 K \((5)\).) The broadening of the left-hand wing of the spectrum points to the formation of a new signal VI. A tenfold increase of the promotor content leads to complete disappearance of signals II, III, and IV (they do not show up after equilibration or evacuation) in \(\text{Ni}(4)-
line{\text{Mo}}(12)/\gamma-\text{Al}_2\text{O}_3\) and the tungsten-containing catalysts. Only signals V and VI are present and especially for the tungsten system it is difficult to estimate the intensity of each signal. The samples \(\text{Ni(Co)}(4)-
line{\text{Mo}}(12)/\text{SiO}_2\) still contain traces of signals II and III but the main contributors to the TNS are signals V and VI.

Since signals II, III, and IV are attributed to paramagnetic sites at the edge surface of the disulfide crystals \((5)\), the results mentioned above are explained by a surface reorganization due to the incorporation of promotor ions in the edges of the disulfide crystals. Farragher and Cossee \((3)\) proposed the decoration model to explain the increase in benzene hydrogenation activity of \(\text{WS}_2\) after addition of small amounts of nickel. The basic idea of this model is a surface reorganization due to a filling of the octahedral holes between the disulfide layers with nickel or \(\text{Ni}^{2+}\) ions, accompanied by an electron transfer from zero-valent nickel to \(\text{W}^{4+}\) ions: \(\text{Ni}^0 + 2\text{W}^{4+} \rightarrow \text{Ni}^{2+} + 2\text{W}^{3+}\). This process is restricted to the edge surfaces for \(\text{WS}_2\) and \(\text{MoS}_2\) \((d^2\) configuration) since the \(d\)-orbital splitting of \(\text{W}^{4+}\) (\(\text{Mo}^{4+}\)) in \(D_{5h}\) symmetry forbids the accommodation of an additional electron. The model is in accordance with the fact that nickel and cobalt influence the ESR spectra of supported sulfided molybdenum and tungsten catalysts essentially in the same way, as is expected from the strong similarity between the crystal parameters of \(\text{WS}_2\) and \(\text{MoS}_2\) as well as between the ionic radii of \(\text{Ni}^{2+}\) and \(\text{Co}^{2+}\).

It is remarkable that the linewidth and \(g\)-value of signal VI for promoted molybdenum and tungsten catalysts are almost the same whereas there are large differences between the ESR parameters of the signals in the unpromoted catalysts (see Table 1). The expressions for the \(g\)-values are determined by the symmetry of the ligand field. The spin–orbit coupling parameter \(\lambda\) and the energy difference \(\Delta\) between the \(d\)-orbital levels are determined by the nature of the ions and the lattice parameters. For signals indicated with the same number the corresponding ligand-field symmetry is expected to be the same. Different \(g\)-values for corresponding signals in molybdenum and tungsten catalysts are thus caused by different values for \(\lambda\) and/or \(\Delta\). The spin–orbit couplings of \(\text{Mo}\) and \(\text{W} d\)-electrons differ and are quite large \((\lambda = 0.11 \text{ and } 0.28 \text{ eV for free } \text{Mo}^{4+} \text{ and } \text{W}^{4+} \text{ ions, respectively} \((10)\)). In solids the value of \(\lambda\) is between 0.50 and 0.85 of the free-ion value \((11)\). For \(\text{MoS}_2\) \(\lambda = 0.09\) has been calculated \((12)\).

The larger value of \(\lambda\) for tungsten compared with molybdenum together with different \(\Delta\) values can explain the larger deviation from \(g = 2.0023\) for the \(g\)-value of signals I and II in tungsten-containing catalysts. The \(g\)-value of signal VI \((2.06 \text{ for } \text{Mo} \text{ and } 2.084 \pm 0.006 \text{ for } \text{W})\) clearly shows that nickel (cobalt) has a very pronounced influence on the paramagnetic centers. Possibly, incorporation of nickel causes a change in \(\Delta\) values of superexchange between nickel and \(\text{W} (\text{Mo})\) occurs.

The linewidth of ESR signals in these samples might be and most probably is determined by dipole–dipole interactions. The linewidth of signal VI seems to depend only on the nature of the promotor ion \((\Delta H = 220 \text{ G for nickel-promoted catalysts and } 320 \text{ G for cobalt-promoted samples})\). The linewidth of the other ESR signals is independent of the presence or absence of pro-
motor ions. The difference in g-value of signal VI for Mo- or W-containing catalysts, together with the fact that signal VI has never been detected in samples containing only promotor ions, leads to the conclusion that the electron giving rise to this signal is primarily located on Mo or W ions.

Since the Curie temperatures of the samples are different it is necessary to calculate the TNS from the reciprocal intensity versus temperature curves. For paramagnetic ions for which the Curie-Weiss law holds, the magnetic susceptibility is

\[ I = \frac{g^2g^*\text{TNS}S(SH)}{3k(T - \theta)} \] (1)

It has been assumed that for all samples the effective spin value \( S = \frac{1}{2} \). From Eq. (1) one can deduce that the TNS is proportional to \( 1/g^2tg \alpha \) (\( \alpha \) is the angle between the 1/I versus I curve in the Curie-Weiss region of Fig. 7). Calibration of the absolute number of spins has been performed by applying this procedure to a Varian Strong Pitch sample. The observed deviations from the Curie-Weiss law in the high-temperature region can be supposed to be caused by a loss of electrons to a higher energy level, for instance the conduction band. The ratio between the electrons in both levels is \( N_2/N_1 = Ze^{\Delta \varepsilon/kT} \) (\( \Delta \varepsilon \) is the energy difference between level 2 and level 1, and \( Z \) is the ratio between the density of states of level 2 and level 1). When \( \Delta \varepsilon \) changes, the temperature domain in which the Curie-Weiss law is obeyed will change.

For tungsten-containing catalysts the difference in Z-values is accompanied by a difference in TNS. A low Z-value gives rise to a high TNS. For molybdenum-containing catalysts lack of data prohibited the calculation of Z-values. It is remarkable, however, that the TNS for alumina- and silica-supported catalysts are of the same magnitude.

The values obtained above for TNS, \( \Delta \varepsilon \), and Z are overall values (the sum of signals II–VI). It is difficult to estimate the contribution of each signal, especially for the broader signals IV–VI. Although the TNS hardly changes after introduction of promotor ions it is clear that the contributing paramagnetic species do change. The surface sites II, III, and IV disappear and VI is formed. Site V, possibly originating from bulk defects, diminishes which could point out a neater crystallization upon introduction of promotor ions. The overlap of signal V with signal VI hampers a quantitative interpretation of the different support dependence of the TNS for molybdenum- or tungsten-containing catalysts. For the molybdenum-containing catalysts it is clear that for Ni(Co)(4)–Mo(12)/SiO\(_2\) signal VI is the main contributor (>75%) to the TNS. The low TNS values for silica-supported tungsten-containing catalysts could be due to larger crystallites compared to alumina-supported samples since silica is a more inert support. The crystallite size and the number of defect structures for molybdenum-containing catalysts are possibly less support dependent. In this re-
specit is noteworthy that for MoS₂ a poorly crystalline structure is known (14).

It is interesting to compare the above results with data reported by Voorhoeve for tungsten-containing catalysts (7). He reported a 10- to 100-fold increase in the TNS as a result of introducing nickel in alumina-supported and bulk WS₂.

The main differences between the present study and Voorhoeve's work have to be found in the ESR spectra of the unpromoted catalysts. The spectra presented here are more complex and probably contain a larger contribution due to bulk defects. The different sulfiding procedure applied here (lower sulfiding temperature, atmospheric pressure) might be the cause of these differences.

**Influence of Equilibration upon the ESR Spectra**

The results obtained with equilibration have to be compared with the evacuation experiments at 673 K with unpromoted catalysts presented earlier (5). While equilibration leads to an intensity decrease of signal II and an increase of signal III, evacuation leads to an intensity decrease of signal II and an increase of signal IV, which is not affected by equilibration. Konings et al. (5) suggested some configurations of atoms at the edges of disulfide crystals, and possible valence and/or symmetry changes upon adsorption and desorption of H₂S in the form of S²⁻ or SH⁻ were given. The combined information from equilibration and vacuum treatment experiments makes it possible to rationalize better the nature of the paramagnetic centers that give rise to the various signals. Depending on whether one deals with a (1010) or a (1010) surface (5, 15) two series of surface atom configurations are possible (see Fig. 8). In the (1010) surface every metal ion has four sulfur ligands that are shared with two other metal ions and two anion coordination sites of its own, while in the (1010) surface two sulfur ligands are shared with two other metal ions and four anion coordination sites are shared with one other metal ion.

The edges of the disulfide crystals consist of an alternate stacking of (1010) and (1010) surfaces. The doubly shared and single-coordination sites can be vacant or filled with S²⁻ or SH⁻ ions. Since signal IV grows upon evacuation and is not sensitive to equilibration it will be associated with surface configurations containing vacancies and sulfur ligands, for instance M³⁺S₄□₂. Signals II and III that disappear upon evacuation and are sensitive to equilibration originate from paramagnetic centers in which several or all vacancies are filled. Most probably type II centers are metal ions, fully coordinated, mainly with S²⁻ ligands, while type III centers may have some vacancies and the other coordination sites filled with SH⁻ groups.

For samples with low promoter content (0.4 wt%) type IV centers are absent and types II and III are the same as for unpromoted catalysts. It is difficult here to draw conclusions about signal VI since signal V (insensitive to evacuation or equilibration) strongly interferes.

**Fig. 8.** Edge structure of WS₂ (MoS₂) crystals.
Samples with a high promoter content (4 wt%) do show a slight change in their ESR spectra upon equilibration. Inspection of Fig. 9 shows that site type VI also has the possibility of having vacancies, $S^2-$, or $SH^-$ ions on the double-coordination sites. Increase of $SH^-$ ligands over $S^2-$ could cause the slight change in ESR parameters.

Voorhoeve (7) reports a strong intensity increase of the ESR signals in promoted catalysts when the $H_2S/H_2$ ratio is lowered. It is argued that the lower the $H_2S/H_2$ ratio is, the more vacancies there are, which should lead to more $W^{3+}$ ions. From the model proposed above it appears that there is no need for a correlation between the $H_2S/H_2$ ratio and the number of $W^{3+}$ ions, since adsorption of $H_2$ and the formation of SH groups will change the tungsten ion valency. Probably different sample conditioning before recording the ESR spectra (evacuation at higher temperatures?) can account for the differences between Voorhoeve's results and the present study.

The formation of metallic nickel observed at $H_2S/H_2 = 10^{-4}$ and 673 K (see Fig. 5c) is in accordance with the phase diagram of nickel sulfide in $H_2S/H_2$ atmosphere (16).

**Influence of CO Adsorption upon the ESR Spectra**

The intensity decrease of signal II (sulfo-$W^{5+}$) and the increase of signals IV and VI (sulfo-$W^{3+}$) can be explained by an electron donation to tungsten ions as a result of CO adsorption. This is in accordance with earlier findings (5): signal II decreases after evacuation at 673 K and after reduction with hydrogen, signal IV increases after evacuation at 673 K. The decrease of signal IV after reduction with hydrogen could be caused by overreduction to $W^{2+}$.

Carbon monoxide has electron-donor properties and direct electron transfer from CO to tungsten or indirect via a decorating nickel ion is a possible reaction. Another possibility is the formation of COS, a reaction that is known to take place over transition metal sulfides (17). This reaction would lead to the donation of electrons:

$$CO + S^{2-} \rightarrow COS_{ads} + 2e.$$

For the unpromoted catalyst the sulfur ions involved in this reaction can only be supplied by the WS$_2$ phase whereas for the promoted catalyst the reaction may also take place over a separated nickel sulfide phase followed by electron transfer to the WS$_2$ phase via conduction. An indication for CO adsorption on WS$_2$ is the observation that the parameters of the ESR signal from the disulfide phase are slightly changed after CO adsorption.

In the presence of nickel an increase in signal intensity after CO adsorption is observed already at 295 K while the unpromoted sample has to be heated to 473 K. In this respect it is noteworthy that especially nickel sulfide and cobalt sulfide have a high activity for the formation of COS (17). These findings suggest that CO adsorption may very well occur on a sulfur ion belonging to the coordination sphere of both a tungsten ion and a decorating nickel ion in case of Ni(4)-W(19.3)/SiO$_2$. Such a sulfur ion would possibly more easily form COS and donate electrons to the disulfide phase.
Activity Measurements

As shown in the literature (8, 18), providing the proper preparation method is applied, highly active HDS catalysts can be prepared on different types of support materials. This is a strong argument for models that ascribe the HDS activity to the presence of the disulfide phase in contrast to the monolayer model, molybdenum with oxygen and sulfur ligands (19, 20).

For silica-supported tungsten catalysts a small amount of nickel (Ni/W = 0.07 atomic ratio) already gives a drastic HDS activity increase. It was found (21) that the thiophene HDS activity increases linearly with the Ni/W atomic ratio in the range 0–0.1 and then stays constant with a decrease at very high nickel contents. This linear increase and saturation at low Ni/W ratio is in accordance with the decoration model (3) while the synergism model (4) predicts a saturation at much higher promotor levels. From the Ni/W ratio at which the level of constant HDS activity is reached, the size of the WS₂ crystallites can be calculated if it is assumed that the decoration model is valid. Figure 9 shows a stoichiometric {10̅10} edge with a sulfur atom ordering that is assumed to be most ideal for benzene hydrogenation (3) and thiophene HDS. One-quarter of the octahedral holes between the disulfide layers are filled with promotor ions, stabilized by six sulfur ligands in this configuration. The number of octahedral holes equals the number of edge tungsten ions (Wₑ), which is related to the total number of tungsten ions (W₁) by: Wₑ/W₁ = 1.26/d (d is the crystal diameter perpendicular to the C axis in nm). Thus d = 0.315 × optimum tungsten/nickel atomic ratio.

For the Ni–W/SiO₂ system a crystallite size of 3.15 nm is thus calculated. This is a very reasonable value and thus in support of the decoration model. In practice there will always be additional promotor ions attached to the carrier and probably in octahedral holes without full sulfur coordination. The calculated value must therefore be regarded as a minimum.

For alumina-supported catalysts the promotor-support interaction prevents the first small amount of promotor ions from decorating the disulfide phase, which explains the equal HDS activities of W(19.3)/γ-Al₂O₃ and Ni(0.4)–W(19.3)/γ-Al₂O₃.

A correlation between thiophene HDS activity or butene hydrogenation activity and the intensity of one of the ESR signals observed, has not been found yet. It is, however, possible that signal VI correlates with the thiophene HDS activity. This signal is absent in unpromoted catalysts, and is the main signal in samples with 4 wt% promoter. As discussed before its intensity in samples with 0.4 wt% promoter is difficult to estimate because of strong overlap with signal V. Future research will be directed to the preparation of catalysts with low signal V intensity, possibly by sulfidation under higher pressure (±10 atm), and catalyst activity tests under medium high pressure.

CONCLUSIONS

The main conclusions of the present work are:

i. Incorporation of nickel or cobalt in supported tungsten- or molybdenum-containing catalysts influences the ESR spectra in a similar way. The results can be best understood in terms of a decoration model.

ii. The intensities of signals II, III, IV, and VI are dependent on the composition of the interacting atmosphere (i.e., equilibration in H₂S/H₂ mixtures, and/or CO adsorption, and/or vacuum treatment). The corresponding paramagnetic centers are most likely situated at the edges of the disulfide crystals.

REFERENCES


