Effect of additives on the CO2 absorption in aqueous MDEA solutions

Citation for published version (APA):

DOI:
10.1021/ie503915k

Document status and date:
Published: 01/01/2014

Document Version:
Publisher’s PDF, also known as Version of Record (includes final page, issue and volume numbers)

Please check the document version of this publication:

• A submitted manuscript is the version of the article upon submission and before peer-review. There can be important differences between the submitted version and the official published version of record. People interested in the research are advised to contact the author for the final version of the publication, or visit the DOI to the publisher’s website.
• The final author version and the galley proof are versions of the publication after peer review.
• The final published version features the final layout of the paper including the volume, issue and page numbers.

Link to publication

General rights
Copyright and moral rights for the publications made accessible in the public portal are retained by the authors and/or other copyright owners and it is a condition of accessing publications that users recognise and abide by the legal requirements associated with these rights.

• Users may download and print one copy of any publication from the public portal for the purpose of private study or research.
• You may not further distribute the material or use it for any profit-making activity or commercial gain
• You may freely distribute the URL identifying the publication in the public portal.

If the publication is distributed under the terms of Article 25fa of the Dutch Copyright Act, indicated by the “Taverne” license above, please follow below link for the End User Agreement:
www.tue.nl/taverne

Take down policy
If you believe that this document breaches copyright please contact us at:
openaccess@tue.nl
providing details and we will investigate your claim.

Download date: 26. Nov. 2019
Effect of Additives on the CO₂ Absorption in Aqueous MDEA Solutions

Maria T. Mota-Martinez,†‡ Sabbir Samdani,† Abdallah S. Berrouk,† Maaike C. Kroon,‡ and Cor J. Peters,§†‡

†Chemical Engineering Department, The Petroleum Institute, P.O. Box 2533, Abu Dhabi, United Arab Emirates
‡Department of Chemical Engineering and Chemistry, Eindhoven University of Technology, P.O. Box 513, 5612 AZ Eindhoven, The Netherlands
§Supporting Information

ABSTRACT: The use of antifoaming and corrosion inhibitor agents to prevent foaming and corrosion, respectively, is widely used in the carbon dioxide (CO₂) absorption process using alkanolamines. However, the effect of these agents on the capacity of the alkanolamine solutions to absorb CO₂ is unknown. We present a study on the phase equilibria and solubility of CO₂ in mixtures of aqueous methyldiethanolamine (MDEA) solutions with and without these additives and show how the liquid phase properties and CO₂ loading capacity is affected.

INTRODUCTION

The use of alkanolamines for CO₂ separation from natural gas is a technology that has been applied since the first patent was granted in 1931. A wide variety of alkanolamines such as monoethanolamine (MEA), diethanolamine (DEA), di-2-propanolamine (DIPA) and n-methyldiethanolamine (MDEA) have been used. The last one, MDEA, is usually preferred when large concentrations of hydrogen sulfide (H₂S) are also present in the gas.

The first description of the use of MDEA in a process to selectively remove H₂S in the presence of CO₂ is given in a publication by Frazier and Kohl. Since then, numerous publications have been reported on the solubility of CO₂ and H₂S in MDEA.

Although the process for CO₂ capture with aqueous alkanolamines solutions is very mature, operating problems are still frequent. The most serious problem of alkanolamine processes is the corrosion, because it compromises not only operation effectiveness but also safety. In addition to selecting suitable equipment materials, corrosion inhibitors are often used during operation.

Foaming is another major issue during operation of an absorption process using alkanolamines. Several causes for foaming formation have been identified, such as the presence of contaminants like liquid hydrocarbons, amine degradation products and other process chemicals including lubricant oil, corrosion inhibitors and suspended particles. Foaming can be prevented by injection of antifoaming agents, which are usually silicones. They are added batch-like to the aqueous amine solution when needed.

The use of corrosion inhibitors and antifoaming agents is very common, but their effect on the CO₂ absorption is not clear and frequently disregarded. In this work, we have studied the effects on the solubility of CO₂ in aqueous MDEA (45.0 mass%) solutions, from a thermodynamic point of view, by addition of these agents.

EXPERIMENTAL SECTION

Materials. The two antifoaming agents were SAG 7133 and VP 5371. SAG 7133 was received in an aqueous solution with 1 part of active component (polydimethylsiloxane) per 9 parts of water (10 mass%), whereas VP 5371 contained 2 parts of active component (organic silicone) per 8 parts of water (20 mass%). Both antifoaming agents were further diluted to 1.0 mass% in water. Therefore, 1 part of SAG 7133 was added to extra 9 parts of water and 1 part of the original VP 5371 solution was diluted in 19 parts of water.

Similar guidelines were followed to prepare the solution with the corrosion inhibitor CRO27005. The aqueous solution containing 1 part of active compound (benzotriazole) per 9 parts of water (10 mass%) was further diluted in 1 part of solution per 19 parts of water.

MDEA was added to the samples, so that in all cases, 45 parts of the amine were present per 55 parts of water.

Experimental Procedure. The effects of additives in MDEA were determined using a synthetic static method, in a so-called Cailletet apparatus. A schematic drawing and a detailed description of this facility can be found elsewhere. The Cailletet apparatus can stand pressures up to 15 MPa and the operating temperature ranges from 275 to 370 K.

Each sample was prepared by placing a well-known amount of the liquid solution in a thick-walled Pyrex glass tube, also referred to as a Cailletet tube. Afterward, the tube was connected to a gas rack, the volume of which had been calibrated. The liquid sample was thoroughly degassed under vacuum conditions before dosing the desired amount of gas (CO₂ in this case). The temperature and pressure in the calibrated vessel was known, so the amount of moles of CO₂...
could be calculated using the virial equation of state truncated after the second term. Mercury was used to push the gas into the Cailletet tube and to seal the sample in its closed top. Besides sealing the sample in the tube, mercury also acted as a pressure transmitting fluid.

The solubility of CO$_2$ in the amine solution has been determined following the bubble point pressure method. This method visually observes the disappearance of the CO$_2$ gas phase by gradually changing the temperature and/or the pressure of the system.

The pressure was generated by pressing hydraulic oil into the system with a screw type hand pump, which caused the level of the mercury column in the Cailletet tube to rise and to create the desired pressure on the sample in the top of the tube. A dead-weight pressure gauge was used to measure the pressure.

The temperature of the sample was kept constant by circulating a thermostat liquid through a thermostat jacket surrounding the Cailletet tube. In this work, water was used, so the temperature range was limited from 280 to 370 K. The surrounding the Cailletet tube. In this work, water was used, so the temperature range was limited from 280 to 370 K. The thermometer in the heat jacket near the top of the sample tube. Homogeneous mixing of the sample was realized by moving a steel ball with two moving magnets.

The uncertainty in the measurements is ±0.005 in the mole fraction of the composition, ±0.01 K for the temperature measurements and the accuracy of the pressure gauge is ±0.01 MPa.

**RESULTS AND DISCUSSION**

**Solubility of CO$_2$ in MDEA Solution.** The Cailletet apparatus has been used for numerous phase equilibrium and solubility studies, the majority of the systems being nonreactive. Although the high accuracy of this apparatus is unquestionable, the applicability to a reactive system was checked. Therefore, the solubility of CO$_2$ in a 45 mass% aqueous MDEA solution was determined and compared with literature data. Four isopleths (lines of constant composition) were measured at four different CO$_2$ loadings ($\alpha = 0.8, 0.9, 1.0$ and $1.5$ mol CO$_2$ per mole of pure MDEA).

The theoretical solubility limit for the absorption of CO$_2$ in the aqueous solution of MDEA is one mole of CO$_2$ per mole of MDEA ($\alpha = 1.0$) according to the data and the chemical reaction model proposed by Jou et al.$^4$

\[
\text{RN} + \text{H}_2\text{O} + \text{CO}_2 \rightleftharpoons \text{RNH}^+ + \text{HCO}_3^-
\]

The results for the solubility of CO$_2$ in the 45% MDEA solution are summarized in Table S1 of the Supporting Information. Figure 1 shows that the samples with a CO$_2$ loadings ($\alpha$) up to 1.0 present a vapor–liquid equilibrium (VLE) curve. As expected, only a vapor–liquid–liquid equilibrium (VLL) was found for the $\alpha = 1.5$ sample, meaning that the loading is beyond the solubility limit of CO$_2$ in the MDEA solution. This can also be noticed from the overlap of the experimental VLL with the pure vapor pressure line of CO$_2$.\(^{12}\)

By fitting the measured isopleths to a third-order polynomial function, the isotherms at 343.15 and 348.06 K were calculated and compared to literature data.\(^{4,13}\) as shown in Figure 2. The data reported in the literature at 343.15 K\(^{4}\) have been used as reference data in handbooks,\(^2\) although it has been claimed that the data of Sidi-Boumedine et al.\(^{13}\) are more reproducible, less scattered and more reliable for modeling.\(^{14}\) The reported values at 348.06 K\(^{13}\) were measured at lower pressures, even below the minimum pressure of the data measured in our system. Nevertheless, both sets of data clearly follow a similar trend, i.e. the data we measured with the Cailletet apparatus agree with literature data.

**Effect of Additives.** The effect of adding antifoaming agents and corrosion inhibitors on the solubility of CO$_2$ in aqueous solutions of MDEA was determined next. Figure 3 shows the evolution of the solution containing any of the antifoaming agents (SAG 7133 or VP 5371) in the Cailletet tube with increasing CO$_2$ pressure. At low pressure (Figure 3a), most of the CO$_2$ is in the vapor phase and the liquid is a homogeneous transparent mixture. As the sample is pressurized (Figure 3b), CO$_2$ starts dissolving in the liquid solution and a second gel-like liquid phase appears, which becomes more pronounced at higher pressures (near the bubble point), as shown in Figure 3c,d. Thus, at the given experimental conditions, CO$_2$ acts as an antisolvent for both antifoaming agents, causing the precipitation of a gel-like silicone-based
substance from the liquid phase. Because antisolvation behavior of pressurized fluids are usually caused by physical interactions, it is expected that the interaction between CO₂ and the antifoaming agents is of physical nature.

To study if the precipitation was caused by the interaction of the antifoaming agent with CO₂ or simply a pressure effect, we prepared a sample with a loading of 0.1 mol of methane (CH₄) per mole of MDEA in the aqueous solution containing the antifoaming agent VP 5371. The formation of the gel-like phase was not observed at any temperature−pressure condition up to 15 MPa. This proves that the interaction with CO₂ and not the pressure effect prompted the precipitation of the silicone-based antifoaming agent.

Precipitate formation did not occur upon addition of the corrosion inhibitor CRO27005 to the MDEA aqueous + CO₂ solution.

Measured results for the effect of adding antifoaming agents and corrosion inhibitors on the solubility of CO₂ in aqueous MDEA solutions at CO₂ loadings of 0.8 and 1.0 can be found in the Tables S2 and S3 of the Supporting Information. Figure 4 shows the bubble point pressure difference (ΔP) between the solutions of MDEA with and without the antifoaming agents or corrosion inhibitor for solutions of 0.8 and 1.0 CO₂ loading.

It has been found that the addition of any of the antifoaming agents increases the bubble point pressure and, as a consequence, the absorption of CO₂ in the aqueous amine solution is negatively affected. On the basis of these data, we estimate that the CO₂ loading in the amine solution is reduced up to 2% when SAG 7133 is added and 1% when VP 5371 is present in the solution.

On the other hand, the solubility of CO₂ in the solution seems to be higher in the presence of the corrosion inhibitor agent CRO27005. Thus, unlike the antifoaming agents, the corrosion inhibitor decreased the bubble point pressure and increased the CO₂ absorption.

**CONCLUSIONS**

The effect of adding the antifoaming agents SAG 7133 or VP 5371 and the corrosion inhibitor CRO27005 on the CO₂ absorption capacity of an aqueous MDEA solution (45%) was studied. It was established that the CO₂ acts as an antisolvent for both antifoaming agents and causes precipitation of the gel-like and silicone-based active agent. The solubility of CO₂ was negatively affected by the addition of both antifoaming agents, whereas the solubility increased when the corrosion inhibitor agent was used.

**ASSOCIATED CONTENT**

Supporting Information
Experimental bubble pressure data of CO₂ + aqueous MDEA solutions with/without additives. This material is available free of charge via the Internet at http://pubs.acs.org.

**AUTHOR INFORMATION**

Corresponding Author
*C. J. Peters. Phone: +971 26075492. E-mail: cpeters@pi.ac.ae.

Author Contributions
The paper was written through contributions of all authors. All authors have given approval to the final version of the paper.

Funding
This work has been financed by the GASCO/ADGAS and the Gas Research Center of the Petroleum Institute in Abu Dhabi.

Notes
The authors declare no competing financial interest.

**ACKNOWLEDGMENTS**

The authors acknowledge the Gas Subcommittee for supporting the project. Prof. Thijs Vlugt and M.Sc. Eugene Straver are especially acknowledged for permitting the use of the Thermolab at TU Delft and their guidance. Maria T. Mota-Martinez is grateful to the Petroleum Institute for the Visiting Graduate Researcher scholarship.
ABBREVIATIONS

$\alpha$ = CO$_2$ loading (moles of CO$_2$ per mole of MDEA)
CH$_4$ = methane
CO$_2$ = carbon dioxide
DEA = diethanolamine
DIPA = di-2-propanolamine
H$_2$S = hydrogen sulfide
MDEA = N-methyldiethanolamine
MEA = monoethanolamine
VLE = vapor−liquid equilibrium
VLLE = vapor−liquid−liquid equilibrium

REFERENCES