Temperature-programmed plasma surface reaction: An approach to determine plasma-catalytic performance

Alexander Parastaeva, Wilfred F.L.M. Hoeben, Bert E.J.M. van Heesch, Nikolay Kosinov, Emiel J.M. Hensen

Inorganic Materials Chemistry Group, Eindhoven University of Technology, 5600 MB Eindhoven, The Netherlands
Electrical Energy Systems Group, Eindhoven University of Technology, 5600 MB Eindhoven, The Netherlands

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ABSTRACT

Plasma-enhanced heterogeneous catalysis offers a promising alternative to thermal catalysis due to the synergy between the plasma and the solid catalyst. However, there is only a limited mechanistic insight about the interactions of highly energetic electrons and excited molecules with heterogeneous catalysts in plasmas. Accurate performance comparison in a plasma-catalytic setting is complicated because of the intricate nature of the plasma-catalyst system: simultaneous reactions occurring in the gas-phase and at the catalytic surface; the dependence of the discharge on dielectric properties of the packed catalyst bed; and the dependence of permittivity and polarization of the catalyst on plasma parameters. Here, we present a method of temperature-programmed plasma surface reaction (TPPSR) that allows decoupling gas-phase processes from the surface plasma-induced reactions. Using this method we reveal the main reasons of apparent synergy between plasma and heterogeneous catalyst for the case of carbon dioxide hydrogenation. Experiments with isotopically labelled CO₂ and temperature-programmed plasma reaction experiments in flow of CO₂/H₂ prove a substantial role of gas-phase dissociation/hydrogenation for the observed catalyst activity and selectivity. The product distribution and reaction pathways do not significantly depend on the discharge parameters. Taking into account overheating of the catalytic bed for comparison of catalytic activity with and without plasma, it was concluded that energy dissipation also plays an important role. The observed plasma enhancement is in part due to the acceleration of electron-induced surface reactions.

1. Introduction

Catalytic hydrogenation of carbon dioxide to methane (the Sabatier reaction) is an important catalytic process. It is applied in the production of synthesis gas, the formation of compressed natural gas [1] and the purification of feedstock for the production of ammonia [2]. The two principle reactions involved are the direct methanation of carbon dioxide and the water-gas shift (WGS) reaction that converts carbon dioxide to carbon monoxide.

\[
\begin{align*}
\text{CO}_2 + \text{H}_2 &\leftrightarrow \text{CO} + \text{H}_2\text{O} \quad \Delta H_{298K} = 42.1 \text{ kJ/mol} \quad (1) \\
\text{CO}_2 + 4\text{H}_2 &\leftrightarrow \text{CH}_4 + 2\text{H}_2\text{O} \quad \Delta H_{298K} = -165 \text{ kJ/mol} \quad (2)
\end{align*}
\]

Non-thermal plasma (NTP) is a promising medium in which to perform catalytic reactions such as CO₂ methanation. Collisions with high energetic electrons in NTP result in ionization and dissociation, and electronic, vibrational, and rotational excitation of neutral reactant molecules [3]. In addition, running a reaction in a plasma can help to overcome thermodynamic equilibrium limitations without heating the system [4]. Many researchers have reported a synergy between heterogeneous catalysts and non-thermal plasma for the reactions of CO₂ conversion. Nizio et al. studied the activity of CO₂ methanation at low temperature in a dielectric barrier discharge (DBD) reactor [5]. Baccariza et al. reported that the promotion of Ni/CsY catalyst with cerium oxide results in an enhanced dielectric properties and higher activity in CO₂ methanation [6]. Improved performance of a Ni/γ-Al₂O₃ catalyst in dry reforming of CH₄ in a low-temperature plasma was mentioned in another study [7]. Wang et al. observed a higher methanol yield in CO₂ hydrogenation over a Cu/γ-Al₂O₃ catalyst in a tailor-made water-cooled DBD reactor at atmospheric pressure and room temperature [8]. Another recent study concerned the one-step plasma-assisted reaction of CO₂ and CH₄ in the presence of noble-metal catalysts, which resulted in enhanced yield of acetic acid, ethanol and methanol [9].

Current mechanistic understanding of the synergy between
heterogeneous catalysts and plasma is very limited. The main challenge is to meaningfully compare catalyst performance in different plasma operation modes and also different catalysts in a plasma. This is difficult because the properties of plasma depend on the filling material (e.g., increasing the dielectric constant enhances the electric field) [10], while the permittivity and polarization of the catalyst is determined by the plasma parameters. Furthermore, unlike in conventional heterogeneous catalysis, comparison of catalysts used in a plasma is complicated by the simultaneous occurrence of reactions at the catalyst surface and in the plasma.

Comprehensive experimental and computational investigation of plasma-catalytic systems is required to gain a better understanding of the interaction between the plasma and the solid catalyst. A number of novel advanced techniques have recently been developed in this area. Isotopically-labeled oxygen was used to study the role of oxygen species in plasma-driven catalysis of volatile organic compound (VOC) oxidation [17,18]. Lee et al. reported that the enhancement of dielectric heating of the catalyst and in this way contribute to a higher apparent catalytic activity. The method is IR thermography. An IR camera in combination with a sap-

2. Experimental

2.1. Catalyst preparation

All chemicals were obtained from Sigma-Aldrich: cobalt nitrate hexahydrate, copper nitrate trihydrate, and nanopowder CeZrO4. A series of CeZrO4 based catalysts with different metals were prepared using a wet impregnation method. For this purpose, the desired amount of metal nitrates was dissolved in 50 ml of deionized water. The suspension obtained by adding 2 g of nanocrystalline CeZrO4 was stirred for 2 h. Then, the water was removed in a rotary evaporator. The cat-

2.2. Catalyst characterization

The crystalline structure of the catalysts was determined by re-

2.3. Catalytic activity measurements

2.3.1. Experimental setup

All experiments were carried out in a tubular DBD reactor made of quartz. The outer diameter of the reactor was 14 mm and the inner diameter 10 mm. The discharge zone in the reactor was 80 mm long and the discharge gap 3 mm. A stainless-steel mesh wrapped around the reactor served as the ground electrode. The inner electrode was a stainless steel rod with a diameter of 4 mm. It was connected to a home-

Overall, novel characterization methods and approaches to compare catalytic performance have to be developed in order to understand the synergism in plasma-catalysis. Here, we present a method called temperature-programmed plasma surface reaction (TPPSR), which is designed to decouple gas-phase processes in a plasma from the processes at the catalyst surface and to properly compare the performance of plasma-catalytic systems. We apply this method and a more con-

A typical discharge pattern (applied voltage and discharge current) for the microsecond pulse source is shown in Fig. 1. Zoomed-in inset for the current waveform shows spikes, attributed to intense
microdischarges observed in the empty DBD reactor. When a catalytic material is introduced inside the plasma reactor, the current waveform is changed significantly Fig. S2. Namely, the current waveform shows microdischarge activity with lower magnitude. In the packed-bed DBD reactor surface discharge and filamentary microdischarges can be generated simultaneously [26,27].

The voltage amplitude was kept constant and the pulse repetition rate was varied to change the energy density. The energy per pulse \( E_p \) (mJ) is calculated by

\[
E_p = \int_{0}^{t_p} V(t)I(t)\,dt
\]

The energy density \( \varepsilon \), (kJ/mol) was used as a parameter to compare the performance of the plasma-catalytic system in CO\(_2\) hydrogenation in a DBD reactor filled with catalyst with an empty DBD reactor. The energy density is defined as the energy deposited into the gas per unit volume and is calculated by

\[
\varepsilon = \frac{E_p V_m}{F}\times 10^{-6}
\]

where \( F \) is the volumetric gas flow through the reactor (L/s) and \( V_m \) the molar volume of gas (22.4 L/mol at 0 °C).

2.3.2. Flow experiments

A variety of reaction experiments with different feed mixtures were performed to investigate the performance of the plasma-catalytic system in CO\(_2\) hydrogenation. In a typical flow experiment, the oven temperature was kept constant and the energy density of the plasma was varied. The pulse duration during the plasma experiments was 90 \( \mu \)s at a frequency 100–1000 Hz. The CO\(_2\)/H\(_2\) ratio was 1/4 at a total flow rate of 25 ml/min.

For experiments with isotopically labelled CO\(_2\), \(^{13}\)CO\(_2\) (99%, Eurisotop) was first pre-adsorbed on the catalyst followed by flushing with a \(^{13}\)CO\(_2\)/Ar mixture. This was followed by a TPR experiment in which we investigated the hydrogenation of gaseous \(^{13}\)CO\(_2\) and adsorbed \(^{13}\)CO\(_2\). In these experiments, the concentration of CO\(_2\) in the gas phase was reduced to 0.3 vol% in order to minimize isotopic exchange.

2.3.3. Temperature-programmed plasma surface reaction

The TPPSR method (schematically shown in Fig. 2) consists of the following steps: (i) adsorption of the reactant on the catalyst surface at ambient temperatures; (ii) flushing of the reactor to remove gas-phase reactant molecules; (iii) exposure of the catalyst to the plasma at ambient temperature to remove weakly adsorbed species and (iv) heating the catalyst to a constant ramp rate in plasma, whilst following the catalytic performance by simultaneous gas-phase analysis by gas chromatography (Shimadzu GC-2014) and mass spectrometry (ThermoStar GSD 320 T2). In the present study, CO\(_2\) was the reactant to be adsorbed on the catalyst, while H\(_2\) was used as a feed during the plasma-catalytic step. The gas hourly space velocity (GHSV) during the adsorption step was set to 400 ml g\(^{-1}\) h\(^{-1}\) and during the TPPSR to 200 ml g\(^{-1}\) h\(^{-1}\). The amount of CO\(_2\) in the gas phase during a TPPSR experiment is much lower than in a conventional experiment when the reactant is part of the feed. Although plasma-induced or thermal desorption of the reactant can lead to a certain concentration of CO\(_2\) in the gas phase as well, we expect the surface plasma-catalytic reactions to dominate the conversion processes during TPPSR experiments.

3. Results and discussion

3.1. Catalyst characterization

The XRD patterns of the CeZrO\(_4\)-supported catalysts are shown in Fig. 3. The diffraction peaks at \( 2\theta = 29.2^\circ, 33.8^\circ, 48.7^\circ \) and \( 57.7^\circ \) correspond to the crystallographic (101), (002), (112) and (103) planes of CeZrO\(_4\) (PDF No. 74-8060). This shows that the material is a homogeneous mixed solid oxide solution of Ce and Zr. Other diffraction peaks belong to copper oxide and cobalt oxide phases dispersed on the support. Using the Scherrer equation, we can estimate the crystallite size of copper oxide to be 28 nm. For 5% Co/CeZrO\(_4\) and 20% Co/CeZrO\(_4\) samples, the average cobalt oxide crystallite sizes are ~21 and ~25 nm, respectively. These results and the metal loadings as determined by elemental analysis are shown in Table 1. The crystallite size of the CeZrO\(_4\) support was about 14 nm for all catalysts. However, on the TEM images acquired for these catalysts (Fig. S3), we can observe that the ceria-zirconia support has a broad particle size distribution up to about 50 nm. It was unfortunately not possible to image Co particles on the CeZrO\(_4\) support by TEM because of the low contrast.

Fig. 4 shows the results of H\(_2\)-TPR characterization of the catalysts. For the copper sample, a significant H\(_2\) consumption was observed at relatively low temperature around 150°C and 220°C. These results are in a good agreement with a previous report for the reduction of copper supported on ceria and ceria-zirconia [28]. The two reduction features can be attributed to reduction of highly dispersed copper strongly interacting with the support and a bulk copper oxide phase, respectively [29]. The reduction of cobalt catalysts correspond to very broad peaks centered around 420°C with shoulders at lower temperature. Bulk Co\(_3\)O\(_4\) reduction usually involves two steps, i.e. Co\(_3\)O\(_4\) → CoO → Co.
The reduction of supported cobalt nanoparticles typically occurs between 300 °C and 400 °C. The higher reduction temperature observed for Co/CeZrO4 likely relates to strong cobalt-support interactions [30].

3.2. Catalytic activity measurements

3.2.1. Flow experiments

As a reference case, we first studied the plasma-assisted hydrogenation of CO2 in a DBD reactor, which was either empty or filled with PbTiO3. The reaction was carried out at 150 °C to avoid condensation of produced water in the system (Fig. 5). The CO2 conversion was not observed in the absence of plasma. The CO2 conversion in the plasma increased proportionally to the energy density. The highest conversion of ∼15% was reached at a frequency of 1 kHz, which corresponds to an energy density of 750 kJ/mol. It is known that conversion and energy efficiency of plasma-catalytic processes can be improved by filling the discharge gap of a DBD reactor with a ferroelectric material, because high dielectric constant leads to the enhancement of the electric field strength [31]. As CO2 does not adsorb strongly on PbTiO3, most of the reaction will occur in the gas phase. CO2 methanation was not observed in the empty reactor nor in the reactor filled with PbTiO3 (Fig. 5a) and the only products were CO and H2O.

We then used a 5% Co/CeZrO4 sample as the catalyst for CO2 hydrogenation. Without plasma, the conversion was about 1% at 150 °C (Fig. 5b). In the plasma, it was found that the CO2 conversion increased with the energy density. The highest CO2 conversion was 70% at a frequency of 1 kHz (energy density of 750 kJ/mol). CH4 was in all cases the main product with a selectivity above 75%. At the highest energy density, the CH4 selectivity was nearly 100%. Similar results were

Table 1

<table>
<thead>
<tr>
<th>Catalyst</th>
<th>Metal loading (%)</th>
<th>Particle size (nm)</th>
</tr>
</thead>
<tbody>
<tr>
<td>CeZrO4</td>
<td>0</td>
<td>-</td>
</tr>
<tr>
<td>5% Cu/CeZrO4</td>
<td>5.0</td>
<td>28</td>
</tr>
<tr>
<td>5% Co/CeZrO4</td>
<td>4.8</td>
<td>21</td>
</tr>
<tr>
<td>20% Co/CeZrO4</td>
<td>20.1</td>
<td>25</td>
</tr>
<tr>
<td>20% Co/CeZrO4 after reaction</td>
<td>-</td>
<td>35</td>
</tr>
</tbody>
</table>

a Determined by ICP.
b Determined by XRD.

The reduction of supported cobalt nanoparticles typically occurs between 300 °C and 400 °C. The higher reduction temperature observed for Co/CeZrO4 likely relates to strong cobalt-support interactions [30].
obtained at 200 °C and very high selectivity to CH₄ was achieved for all values of the energy density.

The synergy between the catalyst and the plasma evident from Table 2 is in line with previous reports [5,8,9]. It results in higher CO₂ conversion at comparable CH₄ selectivity. There are several reasons for these synergetic effects such as plasma-enhanced surface reactions due to high-energy electrons, electric field and radicals on the surface [32]. Another possible explanation relates to processes occurring in the gas phase, for example, dissociation, excitation, ionization of reactants and products [3]. Finally, we should also take into account energy dissipation, which leads to overheating of the catalyst.

3.2.2. TPPR in ¹²CO₂/H₂

In general, TPR is a versatile method to characterize catalytic reactions, for it allows direct comparison of catalysts based on conversion and selectivity as a function of temperature [33]. Here we compared the performance of a 5% Co/CeZrO₄ catalyst in CO₂ methanation in a conventional TPR experiment and a similar experiment with the plasma switched on (TPPR). In both cases, the gas feed consisted of a CO₂/H₂/Ar mixture. For TPPR, we kept the catalyst switched on (TPPR). In both cases, the gas feed consisted of a CO₂/H₂/Ar mixture. For TPPR, we kept the catalyst switched on (TPPR). In both cases, the gas feed consisted of a CO₂/H₂/Ar mixture. For TPPR, we kept the catalyst switched on (TPPR).

The TPR and TPPR results are shown in Fig. 6. In TPR, a broad CO₂ desorption peak at 100 °C is observed. CO₂ reduction starts at 250 °C and CH₄ and H₂O are the predominant reaction products. The trace for H₂O is shifted to higher temperatures in comparison to the CH₄ trace, because H₂O interacts stronger with the catalyst surface. A small amount of CO is also observed at higher temperature.

In TPPR, there is a sharp peak of CO₂ desorption when the plasma is ignited. At the same time, CO formation is observed. It is much higher than for flow experiments at 150 °C and 200 °C in the Section 3.2.1, because at 50 °C methanation activity is low. We attribute CO formation to the dissociation of CO₂ in the gas phase, because CO was also detected as the main product in plasma experiments in the same DBD reactor with and without PbTiO₃. In TPPR, a small amount of H₂O was observed at 50 °C. As low-temperature H₂O formation was not observed in experiments without plasma and H₂O strongly interacts with the CeZrO₂ support, we infer that H₂O is formed due to the reverse water-gas shift reaction on cobalt nanoparticles. Plasma-catalytic enhancement of reverse water-gas shift may be related to dissociation of CO₂ in the plasma.

Comparison of the TPR and TPPR profiles shows that the use of a plasma shifts the temperature of CH₄ formation to lower temperature (from 250 °C to 50 °C). The CH₄ TPPR profile also contains a shoulder in the 50–100 °C range (marked area in Fig. 6b). We link this to the facile formation of CO in the gas phase, which can be formed even in an empty DBD reactor, and its re-adsorption on cobalt nanoparticles leading to further hydrogenation to CH₄.

3.3. TPPR in ¹²CO₂/H₂ with pre-adsorbed ¹³CO₂

Fig. 7a shows the results of an experiment in which ¹³CO₂ was pre-adsorbed on a Co/CeZrO₄ catalyst followed by temperature-programmed reaction in ¹²CO₂/H₂. During the initial isothermal period (50 °C), no ¹³CH₄ was observed. Formation of ¹³CH₄ was seen above 100 °C. On the other hand, ¹²CH₄ was immediately observed in the reactor effluent when the plasma was ignited. This indicates that methanation occurs mainly due to the conversion of gaseous CO₂. We speculate that CO₂ is converted into CO in the gas phase. As CH₄ was not observed in a plasma experiment with an empty DBD reactor nor in a plasma experiment with the CeZrO₄ support, we infer that CO is converted on cobalt nanoparticles. This result also implies that the reaction of CO on cobalt is facilitated by the plasma at low temperature.

Next, we performed a kinetic analysis for the formation of ¹²CH₄ and ¹³CH₄. For this we used leading edge analysis method as introduced by Habenschaden and Küppers [34]. It allows the determination of the activation energy using the leading edge of the temperature-programmed trace. From Fig. 7b, it can also be seen that the apparent activation energies for ¹²CH₄ and ¹³CH₄ formation are similar. This indicates that these products are formed via the same pathway when heating is applied. Therefore, the predominant pathway for plasma-catalytic CO₂ methanation via gas-phase CO was observed only in the isothermal regime at 50 °C.
3.4. TPPSR with pre-adsorbed $^{12}$CO$_2$

Next, we performed TPPSR in a H$_2$ flow with catalysts on which CO$_2$ was pre-adsorbed. This refers to the experiment sketched in Fig. 2. Table 3 shows that the amount of CO$_2$ pre-adsorbed as determined from the breakthrough curves was similar for all three samples. This indicates that CO$_2$ adsorption mostly takes place on the support. Fig. 8 shows product formation as a function of time during the TPPSR experiment for CeZrO$_4$, 5% Co/CeZrO$_4$ and 5% Cu/CeZrO$_4$. For CeZrO$_4$, we observe that ignition of the plasma leads to desorption peaks of a CO$_2$ and CO. As CO$_2$ and CO desorption are nearly instantaneous, it is not likely that these features are due to heating of the catalyst. Instead, we attribute these desorption features to electron impact on the catalyst surface. Adsorption of CO$_2$ on CeZrO$_4$ materials will lead to the formation of various carbonates and formate species [35,36]. Their dissociation upon electron impact may lead to CO$_2$ and CO. Although it is also possible that CO is formed by plasma conversion of desorbed CO$_2$, Fig. 5a shows that the conversion of CO$_2$ to CO in a similar plasma is much lower than in the experiment in Fig. 8a. When the temperature is raised, a new CO$_2$ desorption feature is seen. The amount of CO is much lower, suggesting that most of the formates have already been decomposed at this stage. Above 275 °C, CO formation commences, which is likely due to reverse water-gas shift catalyzed by the CeZrO$_4$ surface. There are only very small amounts of CH$_4$ formed in the isothermal regime and around 400 °C.

When the same experiment is done with 5% Cu/CeZrO$_4$, three CO$_2$ desorption peaks are observed. The amount of CO$_2$ and CO desorbed in the isothermal regime is lower than for CeZrO$_4$, which might be due to the stronger binding of carbonates and formates close to the Cu nanoparticles. Further CO$_2$ desorption occurs in two steps. This can be

![Fig. 6. CO$_2$ hydrogenation in the presence of 5% Co/CeZrO$_4$ catalyst by TPPR method: a) without plasma; b) in plasma, pulse duration 90 μs, frequency 1 kHz. CO$_2$/H$_2$/Ar = 1/4/10, total flow 75 ml/min, heating ramp 10 °C/min.](image)

![Fig. 7. Temperature-programmed hydrogenation of a feed of $^{12}$CO$_2$/H$_2$/Ar (volumetric ratio: 1/100/275; flow rate 75 ml/min) on 5% Co/CeZrO$_4$ on which $^{13}$CO$_2$ was pre-adsorbed. The heating rate was 10 °C/min. The pulse duration was 90 μs at a frequency of 1 kHz, resulting in an energy density of 700 kJ/mol.](image)

<table>
<thead>
<tr>
<th>Catalyst</th>
<th>Results of breakthrough adsorption of CO$_2$ (mmol/g)</th>
<th>Mass balance (%)</th>
<th>Reactor outlet composition (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>CeZrO$_4$</td>
<td>0.160</td>
<td>66</td>
<td>66 31 3</td>
</tr>
<tr>
<td>5% Cu/CeZrO$_4$</td>
<td>0.157</td>
<td>75</td>
<td>32 43 25</td>
</tr>
<tr>
<td>5% Co/CeZrO$_4$</td>
<td>0.161</td>
<td>89</td>
<td>9 3 88</td>
</tr>
</tbody>
</table>

![Table 3. Mass balance and product distribution for the TPPSR catalysts screening.](image)
explained as follows. The onset of the first peak during the temperature ramp is the same as for CeZrO₄. However, CO₂ will be converted via reverse water-gas shift to CO at lower temperature on Cu/CeZrO₄ than on CeZrO₄. We expect that this conversion is predominantly due to the release of carbonates and formates close to Cu particles. This can explain the second desorption peak during the temperature ramp, which is due to carbonate decomposition from parts of the surface where no Cu particles are in close proximity. CH₄ is also formed above 200 °C and the CH₄ trace shows a maximum around 375 °C. The overall CH₄ selectivity for 5% Cu/CeZrO₄ is ~25%, which is much higher than for CeZrO₄. The difference is due to the presence of copper metal.

With 5% Co/CeZrO₄ as the catalyst, CH₄ becomes the dominant reaction product. Whilst CO₂ and CO desorption are observed in the isothermal regime, CH₄ formation already commences at this stage. As already suggested by the results in Section 3.3, this finding implies that CO dissociation and hydrogenation can proceed during the plasma-catalytic reaction. Nevertheless, we should point out that heating of the catalyst cannot be excluded at this stage. In particular, in both of these experiments it is seen that CH₄ formation is delayed compared to CO formation. In the temperature ramping regime, most of the adsorbed CO₂ is converted to CH₄. The CH₄ profile shows a maximum below 200 °C.

Furthermore, the TPPR method allows us to directly compare the activity (Fig. 8a–c) and selectivity (Table 3) of catalysts in a plasma environment. Expectedly, the use of the CeZrO₄ support does not lead to any appreciable CH₄ yield. The main product is CO and CO₂ conversion is rather moderate. Cu/CeZrO₄ exhibits some CH₄ selectivity above 350 °C with higher overall CO selectivity. The most effective catalyst for CO₂ methanation is Co/CeZrO₄ with a total CH₄ yield of ca. 90%. The higher activity of cobalt than copper is in line with known activity trends reported for the Sabatier reaction [1,2,37].

The TPPR method also allows studying the influence of the plasma parameters on the surface processes like plasma-induced desorption and comparing plasma-induced processes to conventional TPR. Fig. 9 shows a comparison between thermal and plasma-assisted desorption of CO₂. In a He flow CO₂ desorption profile has two broad features at 200 °C and 400 °C: a small amount of CO₂ is desorbed at 200 °C and 400 °C. Such strong adsorption can be attributed to the high oxygen storage capacity of CeZrO₄ [38]. Desorption profile of CO₂ in a H₂ flow (Fig. 9b) in the absence of plasma is similar to the experiment in a He flow. The CO₂ desorption peak is centered at 200 °C. Clearly, desorption of CO₂ at 50 °C in the presence of plasma was more pronounced. But the amount of desorbed CO₂ is much smaller compared to the experiment in He flow. Most of the strongly adsorbed CO₂ was reduced to CO₂ and CH₄.

Fig. 8. TPPSR of CO₂ adsorbed on different CeZrO₄-based samples in a H₂ flow: CeZrO₄, 5% Cu/CeZrO₄ and 5% Co/CeZrO₄ at an energy density of 740 kJ/l.

Fig. 10 shows the effect of plasma discharge frequency on the catalytic performance of 5% Co/CeZrO₄ in CO₂ hydrogenation. The temperature maximum of CH₄ production (i.e., catalytic activity) was shifted to significantly lower temperature with increasing discharge frequency. In literature, such an increase in activity upon plasma treatment is usually explained by electron-induced reactions, or the change of catalyst properties in the strong electric field and the formation of radicals on the catalyst surface. However, an effect of catalyst overheating in plasma cannot be eliminated at this stage.

Using the TPPR method, we could also nearly close the mass balance using the breakthrough curves of CO₂ and the total amount of reactants and products leaving the reactor. The adsorbed amounts of CO₂ for 5% Co/CeZrO₄ are displayed in Fig. 5 and similar for all experiments, implying high reproducibility of the measurements. The product distribution and the mass balance for the different experiments without and with plasma are shown in Fig. 10d as well. The identical product distribution in TPPR experiments at different discharge frequencies and without plasma indicates that the mechanism of surface reactions is not changed in a plasma environment, as compared to thermal catalysis. On the contrary, TPPR experiments in a flow of CO₂ and H₂ described in the Section 3.2.2 show significant differences in the product distribution, which proves that the products of plasma-catalysis are very strongly affected by chemical processes occurring in the plasma.

Catalysts with different metal loadings can be also compared by the TPPR method (Fig. 11). The maxima of CH₄ formation are shifted to the lower temperatures with increasing metal loading. This can be explained by the fact that CO₂ pre-adsorbed in close proximity to cobalt particles is easily hydrogenated. It has been shown that CO₂ can be activated on the ceria-zirconia support to form carbonates, which can be further hydrogenated using H atoms deriving from dissociative H₂ adsorption on the supported metal particles [36]. Therefore, a higher metal loading will favor the methanation reaction of adsorbed CO₂.
temperature feature for Co/CeZrO₄, which is most probably due to the formation of carbonates and/or formates strongly bound to the surface of the support. These surface-adsorbed species are the result of oxidative adsorption of CO. This high-temperature feature is absent for Co/SiO₂ because the silica support cannot form these species [36]. Therefore, we can assign the main feature of CH₄ formation, which does not depend on the support, to hydrogenation of CO on the Co metal. Finally, we note that the temperature maximum in CO hydrogenation

Fig. 9. a) CO₂ desorption profile without plasma in helium flow; b) CO₂ desorption profiles in hydrogen plasma under different conditions: 0, 100, 250, 500, 750, 1000 Hz. 5% Co/CeZrO₄ catalyst, pulse duration 90 μs.

Fig. 10. a) and b) CO and CH₄ formation profile at different frequencies: 0, 100, 250, 500, 750 and 1000 Hz; c) Temperature of the maximum CH₄ formation profile; d) Product distribution and mass balance. Catalyst 5% Co/CeZrO₄, pulse duration 90 μs.
depends more strongly on temperature than the temperature maximum in CO₂ hydrogenation.

4. Temperature profiles

The DBD plasma can generally induce dielectric overheating of the catalyst particles and therefore increase the apparent catalytic activity. Some recent publications have described the effect of overheating in plasma-catalysis using an ethanol thermometer [25], XAFS spectroscopy [23], and infrared thermography [24]. To evaluate the impact of dielectric heating on the activity of the catalysts, we measured the temperature profiles by using a conventional thermocouple. We placed a thermocouple into the catalyst bed, and measured the temperature right after the plasma was switched off. A rather significant overheating of up to 100 °C was observed with plasma in the isothermal period (Fig. S5), while without plasma a certain constant lag (∼40 °C) between the oven temperature and the actual bed temperature was observed. Nevertheless, the actual maximum of CH₄ production for conventional heating was approximately at 240 °C, while for the plasma-catalytic process it was about 200 °C, at least 40 °C lower (Fig. 13). Therefore, the observed synergy in plasma-catalytic methanation of CO₂ cannot be explained only by the overheating of the catalyst bed and an actual intrinsic positive effect of plasma is demonstrated. It should also be noted that above 250 °C the temperature with and without plasma is fairly similar. The plasma-induced overheating effect in our DBD reactor mainly takes place in the range from 50 to 250 °C. In any case, temperature measurements for catalytic material in plasma are very important to distinguish the plasma-induced chemical effects and thermal catalysis. It is challenging to measure the temperature of the catalytic bed in a plasma because of limited options for temperature sensors suitable for the high-voltage environment. Moreover, insertion of any temperature sensor inside the plasma-catalytic bed will influence the electric field and discharge properties. Application of pyrometers is also complicated, because ceramic materials, mainly used for DBD reactor (quartz, alumina), are not transparent to the IR light. There is a clear need, therefore, to develop new methods for temperature measurements in plasma-catalytic settings.

5. Conclusions

A new TPPSR method to compare the performance of plasma-catalytic systems was presented. This method can provide a solid understanding of the plasma-catalyst interactions, which can facilitate further development of efficient plasma-catalytic processes. The approach should be applicable to a wide range of plasma-catalytic reactions, such as dry reforming, NOₓ removal, VOC oxidation and CO₂ hydrogenation. Moreover, the influence of dielectric and adsorption properties of
catalytic materials and discharge parameters can be accurately compared with TPPSR. The main requirements for the design of meaningful TPPSR experiments are (i) to avoid extensive conversion of reactants in the gas phase and (ii) to ensure reasonable adsorption of at least one of the reactants on the catalytic surface. We illustrated the potential of TPPSR to decouple the gas-phase plasma processes and the surface plasma-induced reactions in CO2 hydrogenation. Using TPPSR in combination with isotopically labelled CO2, we could understand the role of surface and gas phase processes in Co and Cu catalyzed plasma-enhanced methanation and to assess the impact of plasma parameters on these processes. We also emphasized the influence of plasma-induced overheating as a contributor to the enhanced performance. It was found that the plasma-induced gas-phase dissociation of CO2 favors a low-temperature reaction pathway.

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Appendix A: Supplementary data

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