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## A Theoretical Analysis of Nonsteady-State Oxygen Transfer in Layers of Hemoglobin Solution\*

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**Abstract.** The oxygenation of layers of hemoglobin solutions thick enough to ensure chemical equilibrium between oxygen and hemoglobin has been analyzed theoretically assuming simultaneous diffusion of oxygen and oxyhemoglobin. The dimensionless transfer equation was solved for the finite and semi-infinite situation, the parameters being 1) the ratio of bound to physically dissolved oxygen after equilibration ( $H$ ), 2) the ratio of carrier-mediated to free oxygen flux at steady state ( $D^*$ ), and 3) the dimensionless saturation curve (characterized by  $\Phi_{50}$ ). A parametric analysis provided plots of the dimensionless oxygenation time against these three dimensionless parameters. In this way, from the oxygenation times plotted as a function of the reciprocal oxygen driving pressure in any particular hemoglobin solution, the values of the oxygen permeability (or, knowing oxygen solubility, of the oxygen diffusion coefficient) and of the hemoglobin diffusion coefficient can be derived simultaneously.

**Key words:** Oxygen – Hemoglobin – Diffusion – Facilitated diffusion – Diffusion coefficient of oxygen and hemoglobin.

### Introduction

The theoretical and experimental investigation of the nonsteady-state oxygenation of layers of hemoglobin-containing media is important for many problems of oxygen uptake in the organism as well as in artificial oxygenators. Since the blood is heterogeneous and has a relatively constant composition, studies of hemoglobin

solutions varying in concentration provide a simpler situation covering a wider range of conditions.

The group of Fribourg introduced the thin-layer technique with photometric recording of oxygenation some thirty years ago (review by Kreuzer, 1953). Klug et al. (1956), using the advancing front method, determined the oxygen diffusion coefficient in highly concentrated hemoglobin solution, while taking into account the contribution by the simultaneous diffusion of oxyhemoglobin over the entire range of hemoglobin concentrations for the first time. These studies were extended and confirmed by Kutchai (1971 a, b) who, however, concluded that oxygen diffusion facilitated by oxyhemoglobin was of minor importance only. Spaan (1973) used advancing front equations corrected for the physically dissolved oxygen, and suggested a facilitating contribution by oxyhemoglobin and a possibility of determining values of both oxygen and hemoglobin diffusion coefficients from oxygenation experiments.

Thews (1957) applied an approximate solution of the diffusion equations based on simplifying assumptions to the data of Kreuzer (1950) and Klug et al. (1956) and found good agreement of the values of the oxygen diffusion coefficient between his calculations and previous approaches where a comparison was possible. He neglected, however, the simultaneous diffusion of oxyhemoglobin, as did later studies by Marx et al. (1960), Weissman and Mockros (1969), Dindorf et al. (1971), and Mikic et al. (1972). Moll (1968/69), using numerical methods, on the other hand evaluated the acceleration of oxygen uptake and release by oxyhemoglobin diffusion in red cells.

It is the purpose of the present work to theoretically analyze the oxygenation of hemoglobin solution layers including its facilitation by the simultaneous diffusion of oxyhemoglobin, to compare the theoretical results with new experimental data, and to simultaneously derive the values of the diffusion coefficients of oxygen and hemoglobin over a wide range of hemoglobin

\* Most of this work was performed when the first author was employed at the Biomedical Engineering Section of the Department of Production Engineering, Eindhoven University of Technology, Eindhoven, The Netherlands

solution concentrations in the presence of varying oxygen driving pressures. As may be deduced from the short survey of the literature summarized above, this has never been done before.

In the present first, theoretical, paper the basic relationships are derived based on the diffusion equations for both oxygen and hemoglobin, assuming chemical equilibrium between oxygen and hemoglobin. In a second, companion paper the experimental methods and results will be presented and the most important factors will be derived and discussed.

*The Oxygenation of Hemoglobin Layers of Finite or Semi-Infinite Thickness and the Definition of the Oxygenation Time*

A finite thickness of a flat layer of hemoglobin solution is at one side ( $x = 0$ ) exposed to a gaseous atmosphere and at the other side ( $x = d$ ) limited by a gas-impermeable wall. At time  $t < 0$  the layer is in equilibrium with oxygen at a partial pressure  $P_i$ . The oxygen concentration all over the layer equals  $C_i$  according to Henry's law and the oxygen saturation equals  $S_i$  as required by the oxygen saturation curve. At time  $t = 0$  the gaseous atmosphere is changed abruptly to a  $P_{O_2}$  value of  $P_1$ . Oxygen will diffuse into the hemoglobin layer and react with hemoglobin to produce oxyhemoglobin. We will assume that the reaction of oxygen with hemoglobin is infinitely fast. The transfer equation describing this oxygenation process (Spaan, 1973) is in dimensionless form:

$$\frac{\partial}{\partial t^*} (\Phi + H \Psi) = \frac{\partial^2 \Phi}{\partial x^{*2}} + D^* \frac{\partial^2 \Psi}{\partial x^{*2}} \quad (1)$$

where (see also List of Symbols):

$$t^* = \frac{t D_C}{d^2} = \text{dimensionless time}$$

$$t = \text{time (s)}$$

$$D_C = \text{diffusion coefficient of dissolved oxygen } (\mu\text{m}^2/\text{ms})$$

$$x^* = x/d = \text{dimensionless distance from liquid-gas interface}$$

$$x = \text{distance from liquid-gas interface } (\mu\text{m})$$

$$d = \text{layer thickness } (\mu\text{m})$$

$$\Phi = \frac{C - C_i}{C_1 - C_i} = \text{dimensionless oxygen concentration}$$

$$C_i = \alpha P_i = \text{initial oxygen concentration (mol/l)}$$

$$\alpha = \text{solubility of oxygen in the solution (mol/l/kPa)}$$

$$P_i = \text{initial oxygen partial pressure (kPa)}$$

$$C_1 = \alpha P_1 = \text{final oxygen concentration (mol/l)}$$

$$P_1 = \text{final oxygen partial pressure or oxygen driving pressure (kPa)}$$

$$\Psi = \frac{S - S_i}{S_1 - S_i} = \text{dimensionless oxygen saturation}$$

$$S_i = \text{initial oxygen saturation (fractional)}$$

$$S_1 = \text{final oxygen saturation (fractional)}$$

$$H = \frac{(S_1 - S_i)h}{(C_1 - C_i)} = \text{oxygen concentration ratio} \\ \equiv \text{ratio of bound to physically dissolved oxygen after equilibration}$$

$$h = \text{total oxygen binding capacity of the hemoglobin solution (mol/l)}$$

$$D^* = H \frac{D_H}{D_C} = \text{oxygen flux ratio} = \text{ratio of carrier-mediated to free oxygen flux at steady state}$$

$$D_H = \text{diffusion coefficient of hemoglobin } (\mu\text{m}^2/\text{ms}).$$

The advantage of the dimensionless analysis is that only three parameters are involved ( $H$ ,  $D^*$ , and a parameter defining the dimensionless saturation curve), whereas eight are necessary in the analysis with dimensions ( $D_C$ ,  $d$ ,  $P_i$ ,  $P_1$ ,  $\alpha$ ,  $h$ ,  $D_H$ , and a parameter defining the saturation curve).

The boundary conditions for the finite layer problem are:

$$\begin{aligned} t^* = 0; & \quad 0 < x^* \leq 1; & \quad \Psi = \Phi = 0 \\ t^* \geq 0; & \quad x^* = 0; & \quad \Psi = \Phi = 1 \\ t^* \geq 0; & \quad x^* = 1; & \quad \frac{\partial \Phi}{\partial x^*} = \frac{\partial \Psi}{\partial x^*} = 0. \end{aligned} \quad (2)$$

Profiles of oxygen saturation and oxygen concentration in a finite slab calculated from eqs. (1) and (2) were presented previously (Spaan, 1973). If the hemoglobin is not mobile the saturation profile in general shows a quite steep course, and the profiles are steeper at higher values of  $P_1$ . When hemoglobin is mobile the profiles become smoother, particularly at lower values of  $P_1$ .

In the early phase of the oxygenation process oxygen will not have penetrated into the layer far enough for the boundary conditions at  $x^* = 1$  to influence significantly the distribution of physically dissolved and chemically bound oxygen. Hence one may expect the oxygen uptake of a layer with finite thickness ( $x^* = 1$ ) to be similar to a layer extending into infinity ( $x^* \rightarrow \infty$ ) during this early phase. Note that for this semi-infinite layer the space coordinate  $x$  has been normalized by dividing by the thickness of the finite layer. For the semi-infinite model the third boundary condition of eq. (2) no longer holds and has to be replaced by:

$$x^* \rightarrow \infty: \Phi \rightarrow 0 \text{ and } \Psi \rightarrow 0. \quad (3)$$

It is well known from the analysis of mass and heat transfer problems that for the case of a semi-infinite layer the solution of eq. (1) can be found as a function of only one independent variable  $\eta$  defined by:

$$\eta = \frac{x^*}{\sqrt{t^*}}; t^* > 0, x^* \geq 0. \quad (4)$$

Equation (1) can now be rewritten as a function of  $\eta$  (see Appendix for derivation):

$$-\frac{1}{2} \eta \frac{d}{d\eta} (\Phi + H \Psi) = \frac{d^2 \Phi}{d\eta^2} + D^* \frac{d^2 \Psi}{d\eta^2}. \quad (5)$$

The boundary conditions become:

$$\begin{aligned} \eta = 0; \Phi = \Psi = 1 \\ \eta \rightarrow \infty; \Phi \rightarrow 0 \text{ and } \Psi \rightarrow 0. \end{aligned} \quad (6)$$

This study mainly concerns the increase of the average oxygen saturation when oxygenating hemoglobin layers. The average dimensionless saturation of a finite slab [ $\bar{\Psi}(t^*)$ ] is defined by the ratio of the amount of oxygen already bound to hemoglobin and the maximal amount of oxygen that can be bound to hemoglobin in the layer. This leads to:

$$\bar{\Psi}(t^*) = \int_0^1 \Psi(x^*, t^*) dx^*. \quad (7)$$

In this equation  $\Psi$  is to be calculated by the finite layer model [boundary conditions of eq. (2)]. However, since during the initial phase  $\Psi$  can also be calculated by the semi-infinite layer model, and  $\Psi$  will be practically zero for  $x^* > 1$ , eq. (7) can be rewritten to:

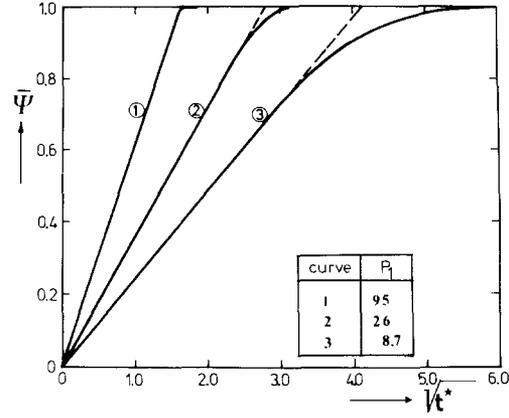
$$\bar{\Psi}_\infty(t^*) = \int_0^\infty \Psi_\infty\left(\frac{x^*}{\sqrt{t^*}}\right) dx^*. \quad (8)$$

The index  $\infty$  indicates that  $\Psi_\infty(\eta)$  ( $= \Psi_\infty\left(\frac{x^*}{\sqrt{t^*}}\right)$ ) and  $\bar{\Psi}_\infty(t^*)$  have been calculated with the semi-infinite model. Obviously we have to restrict the value of  $\bar{\Psi}_\infty(t^*)$  to the physically significant range of  $0 \leq \bar{\Psi}_\infty(t^*) \leq 1$ . With the aid of eq. (4), eq. (8) can be rewritten:

$$\bar{\Psi}_\infty(t^*) = \sqrt{t^*} \left\{ \int_0^\infty \Psi_\infty(\eta) d\eta \right\}. \quad (9)$$

The integral in brackets is independent of time. Hence, according to the semi-infinite model the average saturation has to increase proportionally to the square root of time. For the finite layer this general conclusion only holds as far as the solutions of the finite and semi-infinite layer coincide.

The oxygenation increases of the finite and semi-infinite model are compared in Fig. 1. The range of coincidence of the solutions of both models is considerable and tends to increase as  $P_1$  is higher. This range of coincidence is controlled by the same conditions that make the saturation profile within the layer steeper. This is understandable because the steeper the saturation profile, the longer the profile is "not aware" of the dimension of the layer.



**Fig. 1.** Oxygenation (average dimensionless oxygen saturation  $\bar{\Psi}$ ) of a finite slab as a function of  $\sqrt{t^*}$  ( $\bar{\Psi}_f$ , solid lines) and according to the semi-infinite slab model ( $\bar{\Psi}_\infty$ , broken lines). Oxygen binding capacity  $h = 6.22 \cdot 10^{-3}$  mol/l ([Hb] = 100 g/l),  $D_H/D_C = 0.0281$ ,  $\alpha = 11.4 \cdot 10^{-9}$  mol  $\cdot$  l $^{-1}$   $\cdot$  Pa $^{-1}$ . The oxygen driving pressure  $P_1$  is expressed in units of kPa (1 kPa = 7.5 mm Hg). The finite slab oxygenation was calculated numerically according to Spaan (1973)

Therefore it is permitted to apply the semi-infinite solution throughout a large part of the oxygenation process in layers with finite thickness. During this part of the oxygenation process the average dimensionless saturation increases proportionally to the square root of time as measured continuously over the whole range:

$$\bar{\Psi}_\infty(t^*) = \sqrt{\frac{t^*}{t_1}} = \sqrt{\frac{t}{t_1}} = \sqrt{\frac{t/d^2}{t_1/d^2}} \quad (10)$$

where  $t_1^*$  = dimensionless oxygenation time  
 $t_1$  = oxygenation time  
 $t_1/d^2$  = normalized oxygenation time.

These three interrelated quantities have been defined since  $t_1^*$  is relevant for the dimensionless analysis,  $t_1$  represents the actual oxygenation time of a hemoglobin layer, and  $t_1/d^2$  will be the quantity independent of layer thickness to be measured. Combination of eqs. (9) and (10) results in:

$$t_1^* = 1 / \left\{ \int_0^\infty \Psi_\infty(\eta) d\eta \right\}^2. \quad (11)$$

In the following section a parametric analysis will be performed to evaluate the dependence of  $t_1^*$  on the oxygen concentration ratio ( $H$ ), oxygen diffusion ratio ( $D^*$ ) and dimensionless saturation curve ( $\Psi = \Psi(\Phi)$ ).

The dimensionless dissociation curve is characterized by  $\Phi_{50}$ , the value of  $\Phi$  for  $\Psi = 0.5$ . This  $\Phi_{50}$  is defined by  $P_{50}/P_1$  as long as  $P_1$  is large enough to ensure that  $S_1 = 1$ . Thus with  $P_{50} = 3.55$  kPa (26.6 mm Hg) for the standard dissociation curve a series of curves is obtained for various values of  $P_1$  (Fig. 2). In case of

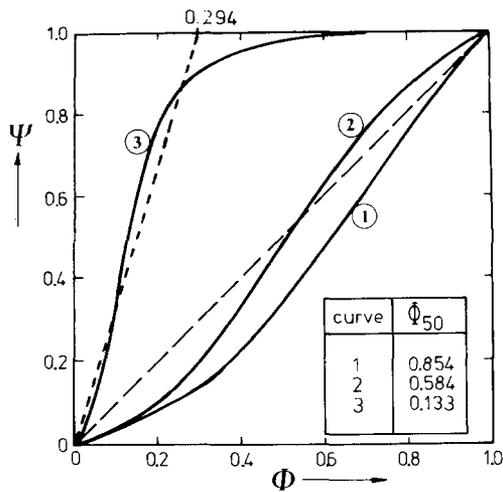


Fig. 2. Dimensionless saturation curves ( $\Psi$  versus  $\Phi$ ;  $P_i = 0$ ,  $\Psi = S/S_1$ ,  $\Phi = P/P_1$ ) at several values of  $\Phi_{50}$ . Every dimensionless saturation curve is obtained from the standard saturation curve and the boundary values  $P_1$  and  $S_1$ . The broken line at the right represents a linear approximation of curve 2, the broken line at the left represents part of the polygonal approximation of curve 3

$S_i = 0$  and  $P_1$  so large that  $S_1 = 1$  the dimensionless saturation curve will have the same shape as the real dissociation curve. When, however,  $P_1$  becomes so small or  $P_{50}$  so large that  $S_1$  is significantly below unity the dimensionless saturation curve will change in shape and  $\Phi_{50} = P_{50}/P_1$  no longer holds. As long as  $S_1 = 1$  the dimensionless saturation curve will be shifted by a change of  $P_1$ , as it will by changing pH,  $P_{CO_2}$  or temperature shifting the real dissociation curve. In Fig. 2 three curves are shown for  $\Phi_{50}$  of 0.854 ( $P_1 = 4.14$  kPa or 31.1 mm Hg), 0.584 ( $P_1 = 6.08$  kPa or 45.5 mm Hg), and 0.133 ( $P_1 = 26.7$  kPa or 200 mm Hg),  $P_{50}$  always being 3.55 kPa (26.6 mm Hg).

Parametric Analysis

A rectangular saturation curve ( $\Phi_{50} = 0$ ) implies the situation of a sharp advancing saturation front. We first studied the influence of both  $D^*$  and  $H$  on  $t_1^*$  assuming a rectangular saturation curve and using the moving boundary model of Hill (1928/1929). The dimensionless oxygenation time obtained with this type of curve will be denoted by  $t_1^{*,0}$  since it forms a certain standard for the oxygenation process at specific values of  $H$  and  $D^*$ . The effects of the saturation curve and of the diffusion of hemoglobin on the dimensionless oxygenation time will be expressed by two factors  $f_1$  and  $f_2$  respectively. Since it appeared that the role of factor  $f_2$  is easily defined for the rectangular saturation curve,  $f_2$  will be discussed first.

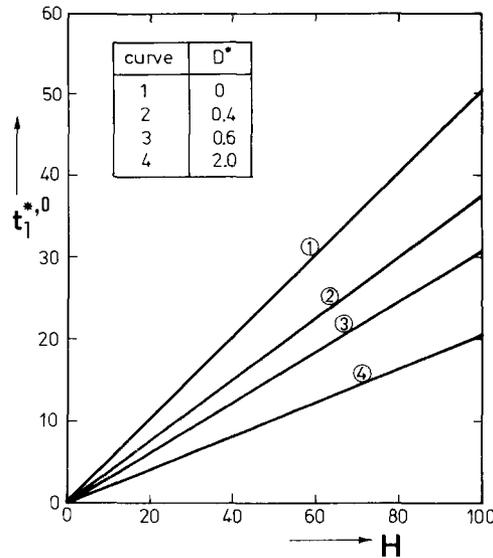


Fig. 3. Dimensionless oxygenation time using a rectangular saturation curve ( $= t_1^{*,0}$ ) as a function of the oxygen concentration ratio ( $H$ ) for four different values of the oxygen flux ratio ( $D^*$ ). The intercepts of the curve with the ordinate are close to zero ( $t_1^{*,0} \approx 0.15$ )

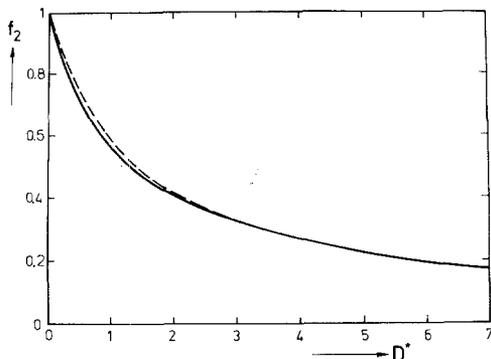
Figure 3 shows that  $t_1^{*,0}$  is a linear function of  $H$  at constant  $D^*$ . The intercept of the curves with the vertical axis is close to zero ( $t_1^* \approx 0.15$ ). In case of  $D^* = 0$  the slope is 0.5 in accordance with the advancing front equation not corrected for physically dissolved oxygen (e.g., Spaan, 1973). Neglecting the small intercept of the curves at  $H = 0$  one may describe the curves of Fig. 3 by:

$$t_1^{*,0} = \frac{1}{2} f_2 H, \tag{12}$$

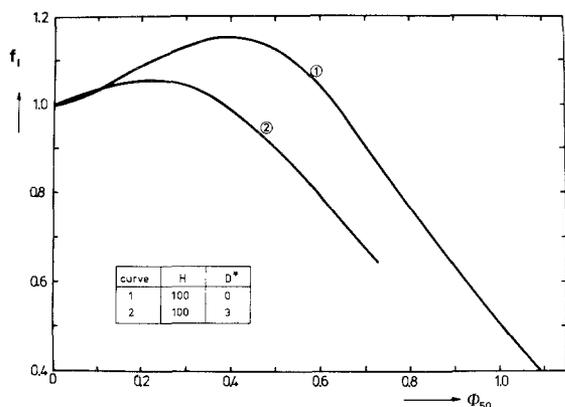
where  $\frac{1}{2} f_2$  is the slope of these curves and depends on  $D^*$ . Indeed,  $f_2$  can be considered as the nonsteady-state facilitation factor reflecting in a reduction of the oxygenation time due to diffusion of hemoglobin.

The nonsteady-state facilitation factor  $f_2$  is plotted in Fig. 4 as a function of  $D^*$ . The curve of  $f_2$  versus  $D^*$  approaches an hyperbolic shape as indicated by the broken line. For  $D^* = 0$  (no facilitation)  $f_2 = 1$ . The total steady-state oxygen flux with boundary conditions at  $x^* = 0$  and  $x^* = 1$  corresponding to the nonsteady-state situation at  $t^* \geq 0$  and  $t^* < 0$  respectively is (e.g. Kreuzer and Hoofd, 1970, 1972):

$$\alpha D_C \Delta P + h D_H \Delta S = \alpha D_C \Delta P \left( 1 + \frac{h D_H \Delta S}{\alpha D_C \Delta P} \right) = \alpha D_C \Delta P (1 + D^*). \tag{13}$$



**Fig. 4.** The nonsteady-state facilitation factor  $f_2$ , being twice the tangent of the relationship between the dimensionless oxygenation time, using a rectangular saturation curve ( $t_1^{*,0}$ ), and the oxygen concentration ratio ( $H$ ) (Fig. 3), as a function of oxygen diffusion ratio  $D^*$  ( $= H D_H/D_C$ ) (solid line). The  $f_2$  versus  $D^*$  curve has a hyperbolic shape and can be approximated (broken line) by  $f_2 = 1/(0.690 D^* + 1)$



**Fig. 5.**  $f_1 (= t_1^*/t_1^{*,0})$  as a function of  $\Phi_{50}$ ;  $t_1^{*,0}$  is the dimensionless oxygenation time for a rectangular saturation curve;  $\Phi_{50}$  characterizes the dimensionless saturation curve. Initially  $f_1$  and thus the dimensionless oxygenation time  $t_1^*$  increase and thereafter decrease with increasing  $\Phi_{50}$ . This behavior is due to the shape of the saturation curve. Curves 1 and 2 differ in the value of  $D^*$  (0 or 3 respectively)

So in fact Fig. 4 relates the nonsteady-state facilitation to the steady-state facilitation.

The influence of the dimensionless saturation curve on the oxygenation time has been studied by plotting the ratio  $t_1^*/t_1^{*,0}$ , called  $f_1$ , as a function of  $\Phi_{50}$  with  $D^*$  and  $H$  as parameters. The oxygenation time  $t_1^*$  was calculated by the semi-infinite layer model. Figure 5 presents two curves for  $H = 100$  and  $D^* = 0$  or  $D^* = 3$  respectively. The ratio  $f_1$  first increases and then decreases with increasing  $\Phi_{50}$  due to the change in shape of the dimensionless saturation curve when  $\Phi_{50}$  increases as shown in Fig. 2 and depends on  $D^*$  except at  $\Phi_{50}$  values below about 0.1. The relationship between  $f_1$

**Table 1.** Dependence of  $f_1 (= t_1^*/t_1^{*,0})$  on  $\Phi_{50}$  for three ranges of parameter values of  $H$  and  $D^*$ . Within these ranges the relationship between  $f_1$  and  $\Phi_{50}$  varies with  $H$  and  $D^*$  within the limits indicated in the table

$\Phi_{50}$	$25 \leq H \leq 100$	$H = 5$	$25 \leq H \leq 175$
	$0.2 \leq D^* \leq 0.8$	$0.2 \leq D^* \leq 0.8$	$D^* = 0$
	$f_1 \pm 0.004$	$f_1 \pm 0.009$	$f_1 \pm 0.002$
0.0191	1.012	1.017	1.002
0.0382	1.018	1.023	1.004
0.0535	1.031	1.043	1.015
0.0891	1.055	1.079	1.029
0.1337	1.077	1.119	1.053
0.2026	1.108	1.181	1.094

and  $\Phi_{50}$  for a given value of  $D^*$  is affected by  $H$  varying from 0 to 500 by no more than 10%.

The influence of  $H$  and  $D^*$  on the relationship between  $f_1$  and  $\Phi_{50}$  was studied in more detail for  $H$  varying between 5 and 175,  $D^*$  varying between 0 and 2, and  $\Phi_{50}$  varying between 0.019 and 0.203. In absolute terms these ranges correspond to hemoglobin concentrations between  $7.7 \cdot 10^{-4}$  mol/l ( $[Hb] = 50$  g/l) and  $4.65 \cdot 10^{-3}$  mol/l ( $[Hb] = 300$  g/l). When the  $P_{50}$  of the saturation curve equals 1.6 kPa (12 mm Hg), as was the case in our experiments, the range of  $\Phi_{50}$  corresponds to  $P_1$  values in the range of 8.3 and 95.8 kPa (62.5 and 720 mm Hg). The results are presented in Table 1 and demonstrate that in the range studied both  $D^*$  and  $H$  have only a minor influence on the relationship between  $f_1$  and  $\Phi_{50}$ .

Figure 5 shows that for  $\Phi_{50} \rightarrow 0$  the numerical solution of the differential equation of the semi-infinite model converges to the solution of the moving boundary equation of Hill (1928/1929) using a rectangular saturation curve as expected ( $f_1 = 1$ ).

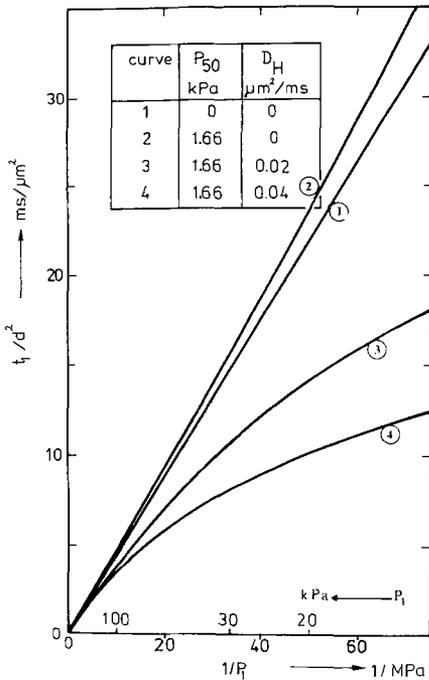
These results may be summarized by the following implicit formula:

$$t_1^* = \frac{1}{2} f_1(\Phi_{50}, H, D^*) f_2(D^*) H. \quad (14)$$

Thus the dimensionless oxygenation time may be expressed as a product of three factors, the oxygen concentration ratio  $H$ , the nonsteady-state facilitation factor  $f_2$  and a factor  $f_1$  describing the influence of the dimensionless saturation curve.

#### *A Strategy for the Experimental Determination of the Oxygen Permeability and Diffusion Coefficient of Hemoglobin in Hemoglobin Solution*

The quantity to be directly measured in oxygenation experiments is the ratio of the oxygenation time ( $t_1$ ) and



**Fig. 6.** The normalized oxygenation time ( $t_1/d^2$ ) as a function of the reciprocal oxygen driving pressure ( $1/P_1$ ) and the influence of both saturation curve and diffusion of oxyhemoglobin on this relationship.  $h = 1.24 \cdot 10^{-3} \text{ mol}/([\text{Hb}] = 200 \text{ g/l})$ ,  $\alpha = 11.5 \cdot 10^{-9} \text{ mol} \cdot \text{l}^{-1} \cdot \text{Pa}^{-1}$ ,  $D_C = 1.2 \mu\text{m}^2/\text{ms}$ ,  $P_{50} = 1.66 \text{ kPa}$ . Curve 1: no influence of saturation curve ( $P_{50} = 0$  and  $D_H = 0$ ); 2: influence of saturation curve and  $D_H = 0$ ; 3: influence of saturation curve and  $D_H = 0.02 \mu\text{m}^2/\text{ms}$ ; 4: as curve 3 but  $D_H = 0.04 \mu\text{m}^2/\text{ms}$

the square of the layer thickness, which is called the normalized oxygenation time:

$$t_1/d^2 = t_1^*/D_C \tag{15}$$

The dimensionless oxygenation time  $t_1^*$  is proportional to  $H$  [eq. (14)] which in turn is proportional to  $1/P_1$  by definition.

The aim of this study is to estimate values for the diffusion coefficients of oxygen and hemoglobin by fitting the theoretically calculated  $t_1/d^2$  to the measured  $t_1/d^2$  for various values of  $1/P_1$ . The dependence of the normalized oxygenation time [eqs. (10) and (15)] on  $1/P_1$  can be obtained by expressing eq. (14) in absolute quantities for the situation where  $S_1 \approx 1$  and  $S_i = 0$ :

$$t_1/d^2 = \frac{1}{2} f_1 \left( P_{50}, \frac{h}{\alpha}, Z D_H \frac{1}{P_1} \right) f_2 \left( Z D_H \frac{1}{P_1} \right) Z \frac{1}{P_1}$$

where  $Z = \frac{h}{\alpha D_C}$ . (16)

When knowing  $P_{50}$  and  $h/\alpha$  the parameters  $Z$  and  $D_H$  can be estimated by the fitting procedure. Accurate knowledge of  $P_{50}$  and  $h/\alpha$  is not needed since  $f_1$  is only slightly influenced by large variations of parameters. However, for the determination of the diffusion coefficient of oxygen from the estimated value of  $Z$ , the

values of  $h$  and  $\alpha$  should be known accurately, whereas for the determination of the oxygen permeability,  $\alpha D_C$ , only  $h$  should be known well.

The characteristic influences of the saturation curve and the diffusion coefficient of hemoglobin on the relationship between  $t_1/d^2$  and  $1/P_1$  are shown in Fig. 6. This figure and eqs. (14) and (16) lead to the following conclusions:

1. If a) there is no influence of the saturation curve on the oxygenation process, b) hemoglobin molecules are immobile, and c)  $P_1$  is varied in a range where  $S_1$  remains close to unity, then the relationship between  $t_1/d^2$  and  $1/P_1$  will be linear (curve 1 in Fig. 6).
2. The influence of the saturation curve, while still assuming  $D_H = 0$ , leads to a concave shape of the  $t_1/d^2$  versus  $1/P_1$  curve (curve 2 in Fig. 6).
3. The carrier facilitation as a result of the diffusion of hemoglobin ( $D_H$ ) leads to a convex shape of the  $t_1/d^2$  versus  $1/P_1$  curve (curves 3 and 4 in Fig. 6).

Thus from  $t_1/d^2$  measured as a function of  $1/P_1$  both the oxygen permeability and the diffusion coefficient of hemoglobin can be derived. However, some difficulties arise at very low  $P_1$  values, e.g., with  $P_1$  less than five times  $P_{50}$ . Figure 1 shows that the linear portion of the plot of  $\Psi$  against  $\sqrt{t^*}$  reaches less far with decreasing  $P_1$  and therefore the determination of  $t_1/d^2$  will be less accurate using the semi-infinite approach. An even more serious reservation against applying low  $P_1$  values is a more marked influence of the saturation curve on the oxygenation process. Referring to Fig. 5, it may be estimated that with  $\Phi_{50} (\approx P_{50}/P_1)$  below 0.2 the term in eq. (16) for the saturation curve ( $f_1$ ) varies by only 5%, i.e., the results will not be much affected by changes or inaccuracies in the saturation curve and  $h/\alpha$ . With lower values of  $P_1$  (i.e., higher values of  $\Phi_{50}$ ), however, the results will be more influenced by the position of the saturation curve. For these two reasons the use of low values of  $P_1$  (high values of  $\Phi_{50}$ ) should be avoided.

The parameter  $Z$  contains the product  $\alpha D_C$  being the permeability for oxygen of the hemoglobin solution. Hence, knowing the oxygen binding capacity of the solution the permeability  $\alpha D_C$  can be derived. The diffusion coefficient of oxygen  $D_C$  can then be calculated knowing the solubility  $\alpha$ .

Figure 4 shows that the sensitivity of the detection of hemoglobin-facilitated oxygen transfer (expressed by  $f_2$ ) depends on the range of  $D^*$ . Due to the hyperbolic shape of the plot of  $f_2$  against  $D^*$  the value of  $f_2$  will change less with altered  $D^*$  in the range of increasing  $D^*$  (which is proportional to  $D_H$  and  $1/P_1$ ).

Based on this analysis and on published values of  $D_H$  a range of  $P_1$  values between 93.1 and 16 kPa (700 and 120 mm Hg), or of  $1/P_1$  values between 10.7 and

$62.5 \text{ MPa}^{-1}$  ( $1.4 \cdot 10^{-3}$  and  $8.33 \cdot 10^{-3} \text{ mm Hg}^{-1}$ ) seems to be an appropriate compromise.

### Evaluation of the "Polygonal Approximation"

When aiming only at an estimate of the values of the physical constants by curve fitting, in general sophisticated theoretical models are not very efficient with respect to computer time. Therefore the polygonal approximation of the saturation curve, as presented by Curl and Schultz (1973) and discussed in more detail by Spaan (1976), has been chosen as a simplified model.

In the polygonal model the saturation curve is approximated by straight line segments. Within these segments  $d^2 \Psi / d\Phi^2 = 0$  (Appendix eq. A6), and the differential equations describing the semi-infinite layer model of oxygen uptake [eq.(5)] can be solved analytically in terms of error functions.

The results of the polygonal model depend on the choice of the approximation of the saturation curve. Curl and Schultz suggested to quantitatively minimize the area between the saturation curve and the straight line segments. However, this suggestion does not always work well as demonstrated by the straight line approximation (broken line) of curve 2 in Fig. 2 according to Curl and Schultz. The computer solution using this curve 2 yields  $t_1^* = 12.7$  ( $H = 100$ ,  $D^* = 3$ ), whereas the straight line approximation yields  $t_1^* = 19.8$ .

In our situation of relatively low values of  $\Phi_{50}$ , the polygonal approximation of the dimensionless saturation curve consists of two segments. The first line originates from the point  $\Phi = \Psi = 0$  and intercepts the line of final saturation  $\Psi = 1$  at the value  $\Phi = \Phi_C$ . The second line continues to the end point  $\Phi = \Psi = 1$ . The value of  $\Phi_C$  (0.2945; see Fig. 2, curve 3) has been chosen such that  $t_1^*$  calculated according to the numerical solution of the semi-infinite layer model equals the value obtained from the polygonal approximation using  $H = 100$ ,  $D^* = 0.6$  and  $\Phi_{50} = 0.1337$ . Any change in  $\Phi_{50}$  was accounted for by a proportional change in  $\Phi_C$  according to  $\Phi_C / \Phi_{50} = 0.2945 / 0.1337 = 2.203$ . This approximate approach holds for the range of  $\Phi_{50}$ ,  $D^*$  and  $H$  pertaining to our experiments to within 1%.

Contrary to previous approaches where the moving boundary equations were derived using the time and place variables separately (e.g. Danckwerts, 1950; Curl and Schultz, 1973; Crank, 1975), the problem is simplified here by combining the dimensionless variables of place  $x^*$  and time  $t^*$  into one single variable  $\eta = x^* / \sqrt{t^*}$ . Due to the early introduction of  $\eta$  the number of physical boundary conditions is restricted since they can only be defined at fixed values of  $\eta$ . Time and place corresponding to fixed values of  $\eta$  are  $x^* = 0$ ,

equivalent to  $t^* = \infty$ , and  $t^* = 0$ , equivalent to  $|x^*| = \infty$ , and moreover those interfaces which change position according to  $x^* / \sqrt{t^*} = \text{constant}$ . The differences in the mathematical treatment of a particular physical problem obviously depend on the specific boundary conditions.

### Conclusions

By comparing the semi-infinite and finite model, the oxygenation process can be described by a single number ( $t_1^* = \text{dimensionless saturation time}$ ), which simplifies the presentation of numerical results. Fortunately the influence of the dimensionless saturation curve ( $\Phi_{50}$ ) appears to be minor and, even better, is uniform over a wide range of values of the oxygen concentration ratio and oxygen flux ratio ( $25 \leq H \leq 100$ ,  $0.2 \leq D^* \leq 0.8$ ) in the range covered. Moreover, in case of a rectangular saturation curve ( $\Phi_{50} = 0$ ) the dimensionless oxygenation time appears to be a linear function of  $H$  for all values of  $D^*$  studied (Fig. 3), where the influence of the oxygen flux ratio ( $D^*$ ) on the dimensionless oxygenation time at  $\Phi_{50} = 0$  ( $= t_1^{*,0}$ ) reflects in the slope of the  $t_1^{*,0}$  versus  $H$  curves. This parametric analysis thus describes the oxygenation process by three diagrams for its dependence on  $H$ ,  $D^*$  and  $\Phi_{50}$  respectively (Figs. 3–5). From these relationships the explicit factors of  $\alpha D_C$  and  $D_H$  may be obtained.

In a companion paper the oxygenation of layers of hemoglobin solutions will be studied experimentally and the determinant factors of this process will be derived.

### List of Symbols

- $C$  =  $C(x, t)$  = oxygen concentration within the hemoglobin layer (mol/l)  
 $C_i$  =  $\alpha P_i$  = initial oxygen concentration (mol/l)  
 $C_1$  =  $\alpha P_1$  = final oxygen concentration (mol/l)  
 $d$  = layer thickness ( $\mu\text{m}$ )  
 $D^*$  =  $\frac{D_H}{D_C}$  = oxygen flux ratio = ratio of carrier-mediated to free oxygen flux at steady state (dimensionless)  
 $D_C$  = diffusion coefficient of dissolved oxygen ( $\mu\text{m}^2/\text{ms}$ )  
 $D_H$  = diffusion coefficient of hemoglobin ( $\mu\text{m}^2/\text{ms}$ )  
 $f_1$  =  $t_1^* / t_1^{*,0}$  = factor characterizing the influence of dimensionless saturation curve on dimensionless oxygenation time (dimensionless)  
 $f_2$  = nonsteady-state facilitation factor (dimensionless)  
 $F$  =  $\int_0^\eta \Psi(\eta) d\eta$   
 $H$  =  $\frac{(S_1 - S_2) h}{C_1 - C_i}$  = oxygen concentration ratio = ratio of bound to physically dissolved oxygen after equilibrium (dimensionless)  
 $h$  = total oxygen binding capacity of the deoxygenated hemoglobin solution (mol/l)  
 $[\text{Hb}]$  = hemoglobin concentration (g/l)

- pH = acidity of the solution  
 $P_i$  = initial oxygen partial pressure (kPa)  
 $P_{\text{CO}_2}$  = partial pressure of carbon dioxide (kPa)  
 $P_{\text{O}_2}$  = partial pressure of oxygen (kPa)  
 $P_1$  = final oxygen partial pressure or oxygen driving pressure (kPa)  
 $P_{50}$  =  $P_{\text{O}_2}$  where hemoglobin is half saturated with oxygen (kPa)  
 $\Delta P$  =  $P_1 - P_i$  = oxygen driving pressure difference across a layer of hemoglobin solution at steady-state oxygen transfer (kPa)  
 $S$  =  $S(x,t)$  = fractional oxygen saturation  
 $S_i$  = initial fractional oxygen saturation  
 $S_1$  = final fractional oxygen saturation  
 $\Delta S$  =  $S_1 - S_i$  = fractional oxygen saturation difference across a layer of hemoglobin solution at steady-state oxygen transfer  
 $t$  = time (s)  
 $t_1$  = oxygenation time defined by semi-infinite layer model (s)  
 $t^*$  =  $tD_C/d^2$  = dimensionless time  
 $t_1^*$  = dimensionless oxygenation time defined by semi-infinite layer model  
 $t_1^{*0}$  = as  $t_1^*$  but applying a rectangular saturation curve ( $\Phi_{50} = 0$ )  
 $t_1/d^2$  = normalized oxygenation time independent of layer thickness  
 $x$  = distance from liquid-gas interface ( $\mu\text{m}$ )  
 $x^*$  =  $x/d$  = dimensionless distance from liquid-gas interface  
 $Z$  =  $h/\alpha D_C$  = parameter to be estimated by fitting theory to experimental  $t_1/d^2$  versus  $1/P_1$  curve  
 $\alpha$  = solubility of oxygen in the solution (mol/l/kPa)  
 $\eta$  =  $\frac{x^*}{\sqrt{t^*}}$  independent dimensionless variable used in the semi-infinite layer model  
 $\eta_C$  = value of  $\eta$  where  $\Phi = \Phi_C$  and  $\Psi = \Psi_C$  in the polygonal approximation  
 $\Phi$  =  $\frac{C - C_i}{C_1 - C_i}$  = dimensionless oxygen concentration  
 $\Phi_{50}$  = dimensionless half-saturation oxygen pressure characterizing the position of the dimensionless saturation curve  
 $\Phi_C$  = abscissa value of intercept point of polygonal approximation of the saturation curve  
 $\Psi$  =  $\frac{S - S_i}{S_1 - S_i}$  = dimensionless oxygen saturation  
 $\Psi_x$  = as  $\Psi$  but calculated according to the semi-infinite layer model  
 $\bar{\Psi}$  = space-average dimensionless oxygen saturation of a hemoglobin layer with finite thickness  
 $\bar{\Psi}_x$  = as  $\bar{\Psi}$  but calculated according to the semi-infinite layer model

## Appendix

The equation holding for the semi-infinite layer model was derived from eq. (1) by the transformation:

$$\eta = \frac{x^*}{\sqrt{t^*}} = \frac{x}{\sqrt{tD_C}} \quad (\text{A1})$$

Because of eq. (A1) one may write:

$$\frac{\partial}{\partial x^*} = \frac{d}{d\eta} \frac{\partial \eta}{\partial x^*} = \frac{1}{\sqrt{t^*}} \frac{d}{d\eta}$$

and

$$\begin{aligned} \frac{\partial^2}{\partial x^{*2}} &= \frac{\partial}{\partial x^*} \left( \frac{1}{\sqrt{t^*}} \frac{d}{d\eta} \right) = \frac{d}{d\eta} \left( \frac{1}{\sqrt{t^*}} \frac{d}{d\eta} \right) \frac{\partial \eta}{\partial x^*} \\ &= \frac{1}{t^*} \frac{d^2}{d\eta^2} \end{aligned} \quad (\text{A2})$$

and also

$$\frac{\partial}{\partial t^*} = \frac{d}{d\eta} \frac{\partial \eta}{\partial t^*} = -\frac{1}{2} \frac{x^*}{\sqrt{t^*}} \cdot \frac{1}{t^*} \frac{d}{d\eta} = -\frac{1}{2} \frac{\eta}{t^*} \frac{d}{d\eta} \quad (\text{A3})$$

Substitution of eqs. (A2) and (A3) into eq. (1) yields eq. (5).

In order to use a standard integration procedure eq. (5) was modified by

$$\frac{d\Psi}{d\eta} = \frac{d\Psi}{d\Phi} \cdot \frac{d\Phi}{d\eta} \quad (\text{A4})$$

and

$$\frac{d^2\Psi}{d\eta^2} = \frac{d\Psi}{d\Phi} \frac{d^2\Phi}{d\eta^2} + \frac{d^2\Psi}{d\Phi^2} \left( \frac{d\Phi}{d\eta} \right)^2 \quad (\text{A5})$$

into

$$\begin{aligned} \frac{d^2\Phi}{d\eta^2} &= \frac{-1}{\left(1 + D^* \frac{d\Psi}{d\Phi}\right)} \frac{d\Phi}{d\eta} \\ &\left[ \frac{1}{2} \eta \left(1 + H \frac{d\Psi}{d\Phi}\right) + D^* \frac{d^2\Psi}{d\Phi^2} \frac{d\Phi}{d\eta} \right] \end{aligned} \quad (\text{A6})$$

For the calculation of  $t_1^*$  the integral  $\int_0^\infty \Psi d\eta$  is needed.

This integral has been solved as follows. First  $F$  is defined as:

$$F \equiv \int_0^\eta \Psi(\eta) d\eta \quad (\text{A7})$$

Twofold derivation of (A7) leads to:

$$\frac{dF}{d\eta} = \Psi(\eta) \quad (\text{A8})$$

$$\frac{d^2F}{d\eta^2} = \frac{d\Psi}{d\eta} = \frac{d\Psi}{d\Phi} \frac{d\Phi}{d\eta} \quad (\text{A9})$$

Eqs. (A6) and (A9) form a set of two differential equations which have been solved simultaneously by a fourth-order Runge-Kutta integration procedure (Library program of the Computing Centre of the Eindhoven University of Technology) resulting in  $\Phi$  and  $F$  as a function of  $\eta$  where  $1/F^2 = t_1^*$  for  $\eta \rightarrow \infty$ .

The integration procedure requires two different boundary conditions per differential equation at  $\eta = 0$ ,

i.e.  $\Phi(\eta = 0)$ ,  $\Psi(\eta = 0)$ ,  $(d\Phi/d\eta)_{\eta=0}$ , and  $(d\Psi/d\eta)_{\eta=0}$ . The latter two replace the physical boundary conditions  $\Phi \rightarrow 0$  and  $\Psi \rightarrow 0$  when  $\eta \rightarrow \infty$ .

The boundary conditions for  $\Psi$  are determined by the boundary conditions for  $\Phi$  by the saturation curve. A parameter estimation program has been developed in order to determine the particular value of  $(d\Phi/d\eta)_{\eta=0}$  satisfying the boundary condition  $\Psi \rightarrow 0$  when  $\eta \rightarrow \infty$ .

All errors involved, including the truncation error by stopping the integration at a finite value of  $\eta$ , add up but remain within  $\pm 0.2\%$  of the calculated value of  $t_1^*$ . For a discussion of this point see Spaan (1976).

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