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Upgrades toward high-heat flux, liquid lithium plasma-facing components in the NSTX-U

M.A. Jaworski\textsuperscript{a,*}, A. Brooks\textsuperscript{a}, R. Kaita\textsuperscript{a}, N. Lopes-Cardozo\textsuperscript{b}, J. Menard\textsuperscript{a}, M. Ono\textsuperscript{a}, P. Rindt\textsuperscript{b}, K. Tresner\textsuperscript{a}

\textsuperscript{a} Princeton Plasma Physics Laboratory, Princeton, NJ, 08543, USA

\textsuperscript{b} TU/Eindhoven, Eindhoven, The Netherlands

Abstract

Liquid metal plasma-facing components (PFCs) provide numerous potential advantages over solid-material components. One critique of the approach is the relatively immature technologies associated with deploying these components in a fusion plasma-experiment. Exploration of the temperature limits of liquid lithium PFCs in a tokamak divertor and the corresponding consequences on core operation are a high priority informing the possibilities for future liquid lithium PFCs. An all-metal NSTX-U is envisioned to make direct comparison between all high-Z wall operation and liquid lithium PFCs in a single device. By executing the all-metal upgrades incrementally, scientific productivity will be maintained while enabling physics and engineering-science studies to further develop the solid- and liquid-metal components. Six major elements of a flowing liquid-metal divertor system are described and a three-step program for implementing this system is laid out. The upgrade steps involve the first high-Z divertor target upgrade in NSTX-U, pre-filled liquid metal targets and finally, an integrated, flowing liquid metal divertor target. Two example issues are described where the engineering and physics experiments are shown to be closely related in examining the prospects for future liquid metal PFCs.

*Corresponding author email: mjaworsk@pppl.gov
1 Introduction

Liquid metal plasma-facing components (PFCs) provide the potential to solve several outstanding issues for solid-material PFCs. A liquid surface is immune to thermomechanical fatigue, which has been shown to produce cracking and morphological changes in tungsten surfaces[1]. The liquid material itself is also immune to neutron damage and the separation of plasma-material interaction (PMI) processes from the structural material allows one to consider a larger breadth of materials as a substrate, such as nuclear-grade steels[2]. The ability to replenish material in real time with controlled flows of the liquid metal would eliminate net-reshaping of the PFCs due to plasma erosion, transport and redeposition[3]. The improved resilience to transient loading and the elimination of the impact of erosion on lifetime of components could relax many of the requirements on divertor operation[4] and Edge-Localized Mode (ELM) mitigation/elimination[5] in present and future devices.

Candidate materials for use as a liquid metal PFC are, in order of increasing atomic number, lithium, gallium and tin. Liquid lithium, in particular, is widely studied for the following reasons: (a) ease of handling as lithium is compatible with steel over a wide temperature range[2], (b) low Z nature has resulted in lower $Z_{\text{eff}}$ of core plasmas[6], (c) the chemical reactivity of lithium to common vacuum system residual gases such as oxygen and water vapor results in reduction of these impurities[7], (d) the chemical reactivity of lithium with hydrogen[8] provides a possible means of fueling control where the inventory of lithium within the machine is also controlled[2], and (e) novel confinement regimes are proposed with the use of very low recycling wall conditions obtained with liquid lithium at low temperatures ($T < 400^\circ\text{C}$)[9]. Lithium also has the highest vapor pressure of the metals listed above which provides an additional erosion mechanism in addition to temperature-enhanced sputtering[10, 11]. The ablation of material at elevated materials is believed responsible for transient vapor shielding during experiments conducted on the QSPA plasma gun device[12]. The exploitation of such high-temperature erosion of liquid lithium PFCs has been proposed to produce a continuously vapor-shielded target[2] that would provide momentum and energy.
losses in a scrape-off layer (SOL) as part of a radiating liquid lithium divertor[13].

The National Spherical Torus Experiment-Upgrade (NSTX-U) has developed a research program that includes a conversion to high-Z components and the eventual testing of flowing, liquid metal modules[14]. The major objective of the research program can be summarized as follows: to establish, experimentally, the difference in operations and performance between a machine dominated by high-Z PFCs or a machine operating with low-Z liquid metal PFCs in a single device. Due to the myriad uncertainties associated with machine variations and the relative paucity of high-power, spherical torii, a single-device experiment seems the cleanest method to establish a clear comparison between these two approaches. In this way, the NSTX-U program will critically evaluate both, the conventional high-Z approach as well as the novel liquid lithium approach. In order to realize this overarching goal, a particular set of upgrades has been begun to develop both the high-Z PFCs as well as the flowing liquid lithium systems. The present work first considers the question of the ultimate temperature limit associated with liquid lithium PFCs. It will then summarize the logic associated with this approach as a means of efficiently upgrading a fusion device for high-Z and liquid lithium experiments. In the course of imagining the upgrade path, certain key experiments will be performed that will inform on the design of liquid lithium PFCs in the future and these will be discussed.

2 The temperature limit of liquid lithium PFCs

A key parameter associated with the operation of a liquid metal PFC is the maximum allowable temperature limit. At very high temperatures, temperature-enhanced erosion and evaporation can greatly increase the loss of material from the surface into the nearby plasma[10, 15]. This, however, is not sufficient to indicate liquid metals in such a state are not viable fusion PFCs. Indeed, it is the goal of numerous research activities to exploit such phenomena to improve the performance of the PFC itself.

Figure 1 shows a schematic diagram of the modes of energy transport available to a liquid
Figure 1: Schematic representation of the modes of energy transport available to liquid metal PFCs. Solid PFCs transfer energy largely via conduction to a coolant. Liquid metal PFCs can transfer energy by phase-change, conduction as well as convective flow and can utilize multiple channels at once.

PFC. Contrasted with solid PFCs, which can only transmit heat by conduction, liquids can utilize both convective transport and phase-change processes to redistribute plasma heat flux. In addition to making use of new channels, many liquid metal concepts attempt to utilize multiple energy transport channels. For example, the proposed, actively-supplied, capillary-restrained scheme would utilize both phase-change (including radiation from the resulting lithium vapor-cloud) as well as conduction cooling to a conventional coolant such as helium or some other fluid[2]. Realizing large densities of lithium in the plasma from evaporation or other processes that intentionally inject lithium may require some form of trapping or differential pumping. One implementation of such a scheme has been called a “vapor-box” system[16]. This scheme would make use of dissipative processes to redistribute plasma heat-flux more uniformly within the divertor region. Heat is then exhausted to a conventional coolant. Surface lithium temperatures over 900°C may be required to realize the full potential of the concept.

Similar surface temperatures can significantly increase the effectiveness of liquid metal
concepts utilizing fast-flow to convect heat away from the strike-point region. Consider a stream of liquid moving under a uniform heat flux as an approximation of a divertor strike-point impinging a fast-flowing liquid metal. If one considers the liquid metal flow as largely laminar due to the suppression of turbulence by MHD effects[17], then one model for the system is that of a moving slab of material. If the thickness of the fluid flow is larger than the thermal penetration depth, then the temperature rise can be approximated as for a semi-infinite solid:

\[ \Delta T(t) = 2 \frac{q_0 \sqrt{\alpha t}}{k \sqrt{\pi}} \]  

where \( \Delta T(t) \) is the surface temperature rise as a function of time, \( q_0 \) is the incident heat flux, \( \alpha \) is the thermal diffusivity of the material, and \( k \) is the thermal conductivity. The time of exposure, \( \tau_{\text{transit}} \) can be related to a characteristic length-scale in the divertor, \( L_{\text{char}} \) and the velocity of the liquid metal, \( v_{LM} \) through that region as \( \tau_{\text{transit}} = L_{\text{char}} / v_{LM} \). The allowable temperature rise, \( \Delta T_{\text{LIM}} \) is a function of the limiting temperature for operation in the fusion device and the injection temperature. Rearranging terms, one can solve for the exhaust capacity of the flowing liquid:

\[ q_0 = \frac{\Delta T_{\text{LIM}} k \sqrt{\pi v_{LM}}}{2 \sqrt{\alpha L_{\text{char}}}} \]  

Figure 2 evaluates eq. 2 as pertains to a fast-flowing liquid lithium stream for different values of a limiting surface temperature from 400–900°C. As can be observed, a higher limiting surface temperature can either relax the requirements on flow velocity or increase the heat-exhaust capacity.

3 Prospects for high-temperature lithium PFCs

These analyses highlight the need to identify the ultimate temperature limit of a liquid lithium surface to know what will be compatible with a given plasma scenario (e.g. H-mode) or configuration (e.g. diverted). Understanding the compatibility of this novel regime will
depend on addressing the fundamental processes governing material transport in the SOL. A brief overview of available literature will be presented as well as experimental results from studies conducted on the Magnum-PSI linear plasma device[18].

The strong temperature-dependent erosion yields from liquid lithium surfaces results in many investigators generating maximum temperature limits for this material. Rognlien and Rensink assumed isothermal wall and divertor conditions with 2-D modeling with the UEDGE code and obtained a temperature limit of 370°C[19]. Arguments based on a 1% limit on impurity influx limit create a temperature limit for liquid lithium of approximately 400°C though this particle balance criteria is also affected by local redeposition which can extend the allowed temperature range[20]. Both of these works utilize Langmuir law models to describe the evaporation rate of the lithium into the nearby plasma. Experimental work with lithium limiter targets have demonstrated operation of the limiter above 550°C before disruption on the FTU tokamak[21]. Consideration of momentum balance in a tokamak SOL yields different results than particle flux estimates. In the case of experiments in the NSTX with measured target plasma electron pressures of 100-200 Pa, the corresponding equilibrium vapor pressure of lithium is reached at approximately 750°C[2]. Reactor pressures would be expected to reach above 6 kPa which suggests surface temperatures above 900°C[16]. This
wide temperature uncertainty demands experimental verification and would have significant implications on the maximum heat-flux limits of liquid lithium PFCs as well as the efficiency of thermal power cycles interacting with those PFCs - hence this is a key parameter to be examined by the NSTX-U research program. Already there are indications that previous estimates require revision as evidenced by experiments re-examining the lithium erosion yield in high-flux deuterium plasmas[22] and the resulting changes in deuterium transport at high lithium-deuteride concentrations[23]. Two effects are observed in these recent experiments: first, the gross erosion rate is found to be reduced below experiments conducted in low-flux devices and second, a high redeposition rate was calculated indicating strong trapping at the surface[24].

4 The upgrade path to flowing liquid metal modules

The NSTX-U is the newest large-scale fusion experiment to come online in the US[25]. The major elements of the upgrade include a second neutral beam heating system and an improved center-stack. The center-stack upgrade enables toroidal fields of 1 T, plasma currents of 2 MA and pulse-lengths of 5 s. The second neutral beam heating system effectively doubles the available input power resulting in a maximum available heating capacity of 19 MW. These upgrades place NSTX-U in a unique position relative to other fusion devices world-wide. Two metrics of interest are the \( P/R \) and \( P/S \) parameters of each machine meaning the available input power, \( P \), divided by the machine major radius, \( R \), or the machine surface area, \( S \). Table 4 provides a comparison of NSTX-U with a number of machines current or planned. The compact, high-\( \beta \) nature of the NSTX-U makes it possible to reach very high values of both metrics.

Another feature of the NSTX-U is the open floor divertor configuration. This divertor, while sacrificing the dissipative benefits of a closed divertor, makes it possible to explore a wide variety of different plasma shapes and PFC options. Already, the NSTX had made use of this flexibility in testing the Liquid Lithium Divertor (LLD)[26, 27]. This high-Z PFC
Table 1: Multi-machine comparison of size and various power-exhaust metrics. ST-Pilot and ST-DEMO pulse lengths given in terms of discharge-seconds per year.

<table>
<thead>
<tr>
<th>Machine</th>
<th>$R_0$ (m)</th>
<th>$P_{\text{Aux}}$ (MW)</th>
<th>$P/R$ (MW/m)</th>
<th>$P/S$ (MW/m²)</th>
<th>$\tau_{\text{pulse}}$ (s)</th>
</tr>
</thead>
<tbody>
<tr>
<td>NSTX*</td>
<td>0.86</td>
<td>6.8</td>
<td>8</td>
<td>0.2</td>
<td>1</td>
</tr>
<tr>
<td>NSTX-U*</td>
<td>0.93</td>
<td>19</td>
<td>21</td>
<td>0.6</td>
<td>5</td>
</tr>
<tr>
<td>JET†</td>
<td>2.95</td>
<td>35</td>
<td>12</td>
<td>0.2</td>
<td>20</td>
</tr>
<tr>
<td>DIII-D†</td>
<td>1.74</td>
<td>20</td>
<td>11</td>
<td>0.4</td>
<td>6</td>
</tr>
<tr>
<td>AUG†</td>
<td>1.65</td>
<td>27</td>
<td>16</td>
<td>0.6</td>
<td>10</td>
</tr>
<tr>
<td>CMOD†</td>
<td>0.7</td>
<td>6</td>
<td>9</td>
<td>0.7</td>
<td>2</td>
</tr>
<tr>
<td>MAST†</td>
<td>0.87</td>
<td>7.5</td>
<td>9</td>
<td>0.25</td>
<td>1</td>
</tr>
<tr>
<td>ITER†</td>
<td>6.2</td>
<td>100</td>
<td>16</td>
<td>0.15</td>
<td>400</td>
</tr>
<tr>
<td>ST-Pilot‡</td>
<td>2.2</td>
<td>190</td>
<td>86</td>
<td>0.7</td>
<td>$6 \times 10^6$</td>
</tr>
<tr>
<td>ST-DEMO‡</td>
<td>3.2</td>
<td>520</td>
<td>161</td>
<td>0.9</td>
<td>$\infty$</td>
</tr>
</tbody>
</table>


A similar logic is proposed for upgrading the NSTX-U to all high-Z. Beginning with experimental operations in 2015, the NSTX-U will begin with a return to all graphite surfaces. PFC upgrades will initially be placed at an outboard location to preserve experimental capabilities as was done in the case of the LLD. In addition, the PFC upgrades themselves will be interchangeable with the graphite surfaces. Over the course of approximately five years, the machine would be converted to all, high-Z PFCs beginning with a portion of the outboard divertor, to complete conversion of the outer half of the lower vessel, extending
then to include the outer and inner first-wall PFCs, and then finally the remaining lower and upper divertor areas will be converted. This plan retains graphite in the highest heat flux areas for a maximum amount of time due to its robust performance as a PFC.

Just as the upgrades to the in-vessel PFCs is staged, implementation of a flowing liquid lithium module would be difficult to realize in a single step. Instead, portions of the technology are implemented in steps to confirm engineering design and analysis of the PFCs. The major elements required for a confinement device, liquid metal PFC are shown in figure 3. Six major elements are expected to be required in creating an integrated module with flowing liquid metal for the divertor of a confinement device. Beginning in the top left of the figure and proceeding counter-clockwise these are described as follows:

1. the PFC structure itself must be capable of absorbing, or otherwise intercepting a significant (i.e. divertor-relevant) heat flux and dissipating it or otherwise avoiding permanent damage,

2. the PFC substrate and structure itself must withstand thermomechanical and electromagnetic loads, the PFC substrate material itself must be chemically compatible with the liquid metal in the expected temperatures of use,

3. the liquid metal must adhere to the surface of the substrate in order to be wetted and maintain coverage of the PFC itself,
4. technologies necessary to moving the liquid metal throughout a system and into and out of vacuum must be developed and demonstrated in order to be integrated into a flowing system,

5. safety systems and procedures associated with the liquid metal handling technologies as well as in-vessel components must be established, and

6. plasma scenarios and operational control needs to be developed to account for the changes that may arise with the use of the liquid metal PFC.

While significant development on most of these items can be accomplished in a laboratory environment, item #6 explicitly requires a confinement device. In addition, the operation of a confinement device with a high-vapor pressure divertor target is, it must be admitted, a speculative concept at present. Implementation of a fully-flowing module that will not be able to operate in the relevant temperature regime associated with good confinement could lead away from some liquid metal concepts and emphasize others. In the extreme, for instance, if high-temperature lithium could not be used and divertor heat-fluxes could not be reduced, then a fast-flowing system would be required which, technologically, is a significantly different design than slowly-flowing or oozing systems.

Balancing all these needs, the approach currently favored for the NSTX-U program is a set of incremental upgrades that will, in turn, establish the feasibility of new operating scenarios while gradually increasing the complexity of the liquid metal system. These upgrades involve the following:

1. a continuous row of high-Z PFC tiles in the NSTX-U divertor,

2. the implementation of pre-filled, liquid-metal PFC target tiles in the same region, and

3. a fully-integrated, flowing liquid metal system

Each of these upgrades will address certain key technological and scientific questions described next.
4.1 High-Z divertor target upgrade

The first major upgrade is the high-Z PFC tile upgrade for the NSTX-U divertor. The current PFCs are composed of an amorphous graphite (type “ATJ” manufactured by Union Carbide). Upon application of a lithium layer, the lithium rapidly diffuses (or “intercalates”) into the graphite resulting in a loss mechanism not related to plasma erosion or evaporation[28]. Experiments comparing lithium coating lifetimes on graphite vs. a molybdenum alloy (TZM) substrate found a factor of 100 change in the available lithium at the surface of the substrate[24]. This indicates that the metallic substrate will serve as a more substantial source of lithium for plasma experiments than would be expected from graphitic surfaces. In addition, the high-Z tiles will provide a compatible substrate that can resist the thermomechanical and electromagnetic forces it will be subjected to during plasma bombardment at divertor-relevant heat fluxes. The high-Z divertor tile surfaces are expected to reach over 1200°C during experiments placing the strike-point directly on the high-Z tiles - cooling is by thermal inertia.

Lithium will continue to be applied by evaporation from the NSTX LITER systems[29]. Experiments conducted in the Magnum-PSI on evaporated coatings on TZM molybdenum found significantly suppressed erosion rates under high-flux deuterium bombardment[22]. The first experiments in NSTX-U will provide a confinement-device analogue to these experiments to confirm whether the gross erosion is suppressed. Very high redeposition rate, \( R > 0.99 \), indicating a strong trapping effect at the PFC surface. Repetition of these conditions in the tokamak will compare the normal-incidence magnetic field experiments in Magnum-PSI with oblique-incidence magnetic field conditions found in a tokamak divertor. These experiments at high-temperatures will begin to address the overall plasma-compatibility (e.g. confinement properties) with these limited-inventory, lithium coatings on high-Z substrates.
4.2 Pre-filled liquid metal divertor targets

The second major upgrade and experiment will involve a novel PFC system: a pre-filled liquid metal target. In concept, these devices are similar to Capillary-Porous Systems developed in the Russian Federation[30] and deployed on several devices[6]. A schematic of such a PFC target is shown in figure 4. The key difference between this present concept and that of a CPS is that we are targeting a divertor-relevant PFC whereas CPS devices are inserted as movable limiter probes. At a high level, then, the PFC would include an internal liquid metal reservoir and a wicking structure to allow transport of material from the internal spaces to the free-surface. Wetting and spreading on the surface is enhanced by surface texturing. As with the high-Z divertor upgrade, heat-flux handling is primarily through thermal inertia and similar temperature would, in principle, be feasible. Technologically, this upgrade will achieve the introduction of lithium into the NSTX-U without the use of the LITER evaporation system and realize the production of a complex, liquid metal PFC divertor target.

Scientifically, the prefilled targets will be used to establish the viability of passive-replenishment strategies for the slowly-flowing concepts. It will also further establish the compatibility of high-temperature lithium targets with the plasma. In contrast the experiments on the high-
Z tiles previously described, the prefilled targets will each have reservoir capacities in the several grams of Lithium range whereas the entire vessel deposition with the LITER system is on the order of 100–500 milligrams. In other words, the limited inventory of evaporated coatings may provide an optimistic assessment of high-temperature lithium compatibility whereas a pre-filled target will more closely mimic a fully-flowing system in available lithium inventory.

4.3 Fully-integrated, flowing divertor targets

As a final upgrade, liquid metal handling technologies would be integrated to the confinement device PFCs creating a fully-flowing, liquid metal PFC. Technologically, if internal cooling is not included, then already the pre-filled target schematic looks similar to actively-cooled concepts shown in ref. [2]. If inertial cooling is again utilized, then the integrated PFCs will look, in concept, very similar to the pre-filled targets. In the context of the NSTX-U where only 5 s discharges are planned in the near-term, inertial cooling should be sufficient for experiments. For an oozing-flow system, techniques will have to be developed to re-collect excess fluid that has passed over the PFC or deposited onto other surfaces.

Scientifically, one would expect most of the questions of plasma compatibility to have been addressed with the pre-filled targets. However, integration with a liquid-metal pumping system provides the ability to enhance the passive replenishment of liquid metal with active means (i.e. pressurization). An important goal for this stage of the project would be an assessment of the liquid metal inventory, transport and control during normal and off-normal plasma operations. Such inventory control would be essential for future reactor concepts[2].

5 Experimental interpretation and design of components

Two example research problems detailing particular questions facing the high-Z divertor and pre-filled target experiments are included. These samples are included in that they pertain specifically to a high-temperature development program and one where sacrificial
layers are emphasized. Additional research and experiments will further explore issues related to interpretation and conduct of experiments. In particular, these two elements highlight some of the difficulties in engineering design of these components and how they impact the scientific program and vice versa.

5.1 Leading edge effects on lithium experiments

An inhomogenous divertor target will produce leading edges in the absence of special geometries such as fish-scaling. The NSTX-U divertor is composed of divertor tile targets that do not have fish-scaling geometries in order to preserve the capability of operating with the toroidal magnetic field in the opposite direction. As a result, some attention is necessary to the production and mitigation of leading-edge effects.

A schematic view of the geometry involved at a gap between divertor PFCs is shown in figure 5. The magnetic field line is incident on the nominal PFC surface at an angle $\alpha$ to the surface. As expected, for a nominal parallel heat flux, $q_\parallel$, the surface heat-flux, $q_0$ is related to $q_\parallel$ by the total angle of incidence as

$$q_0 = q_\parallel \sin(\alpha)$$

(3)

Typical divertor angles of incidence are in the range of 1–5°. At a sharp corner, then, the
angle changes to $\alpha + 90^\circ$ resulting in $q_0 \simeq q_{||}$. This region of enhanced heat flux is limited in area, but can lead to significant heating of the leading edge, even for relatively small values of gap space, $g$.

One mitigation strategy is to eliminate the leading edge by introducing a chamfered edge as shown in figure 5. This chamfer geometry eliminates the leading edge at the cost of an increased total angle, $\alpha + \theta$ on the following chamfer face. For small angles, the enhancement in heatflux over the nominal front-face heat flux, $f_{enh}$ is given as follows:

$$f_{enh} = \frac{q_{||} \sin(\alpha + \theta)}{q_{||} \sin(\alpha)} \simeq \frac{\alpha + \theta}{\alpha} \quad (4)$$

In the case that a single angle of incidence is known and the gap, $g$ is known, then the chamfer width, $c$, and depth, $d$ can be calculated to exactly shadow the next leading edge:

$$c = \frac{g \tan(\alpha)}{\tan(\theta) - \tan(\alpha)} \quad (5)$$

$$d = c \tan(\theta) \quad (6)$$

In practice, however, manufacturing tolerances will add to both the gap size as well as introduce a potential vertical displacement. In addition, a range of values for $\alpha$ can be imagined as a result of different tokamak geometries during experiments.

A theoretical minimum exists in which the trailing edge chamfer angle exactly equals in the nominal angle of incidence leading to $f_{enh} \geq 2$. In practice, accounting for finite tolerances, values of $f_{enh} \simeq 2.3$ are typical. From eq. 5 one can see that as the chamfer angle, $\theta$ approaches the value of $\alpha$ the width of the chamfer, $c$, grows large — another practical issue that limits the value of $f_{enh}$. Values of less than two can be achieved in alternate geometries such as a ramped scheme variation but this does not support bi-directional operation.

While these relationships are fairly standard in the field, there is a particular impact the leading-edge heating effects have in the context of lithium experiments. The temperature rise on the PFC surface scales as the incident heat flux (c.f. eq. 1). The surface average
Figure 6: The surface average temperature as a function of chamfer enhancement factor at different chamfer fractional areas.

The surface average temperature, $< T >$, including increases due to the presence of chamfer features can be calculated as follows:

$$< T > = \frac{A_{nom}T_{nom}}{A_{div}} + \frac{A_{ch}T_{enh}}{A_{div}} = (1 - f_{ch})T_{nom} + f_{ch}T_{enh}$$  \hspace{1cm} (7)

where $A_{nom}$, $A_{ch}$, and $A_{div}$ are the total nominal (flat) surface area, the total chamfer surface area and the total divertor surface area respectively. The fraction of surface area at an enhanced temperature is $f_{ch} = A_{ch}/A_{div}$. The nominal surface temperature is $T_{nom}$ whereas the temperature on the chamfer surfaces is $T_{enh}$. As it is the temperature rise that scales with incident heat flux, the enhanced temperature due to a given heat flux enhancement factor is given as:

$$T_{enh} = T_0 + f_{enh}\Delta T_{nom}$$  \hspace{1cm} (8)

whereas $T_{nom} = T_0 + \Delta T_{nom}$ with $T_0$ being the initial temperature. Figure 6 shows the relationship between the surface average temperature and the heat-flux enhancement factor for a range of values of $f_{ch}$.

While the surface average temperature is a completely linear relationship, there is an additional effect to consider when conducting lithium experiments. In the case of a surface
covered in a liquid, the evaporative flux, \( J(T) \) is calculated from as follows[31]:

\[
J(T) = \frac{P_v(T)}{\sqrt{2\pi mkT}}
\]

(9)

where \( P_v(T) \) is the equilibrium vapor pressure at temperature \( T \), \( m \) is the atomic mass of the liquid, and \( k \) is the Boltzmann constant. The vapor pressure of lithium in Pascal is given as[32]:

\[
P_v(T) = 133.3 \exp\left(18.4 - \frac{18750}{T}\right)
\]

(10)

where \( T \) is expressed in Kelvin.

The surface flux of material, \( \langle J \rangle \), due to evaporation can be constructed as follows:

\[
\langle J \rangle = J(T_{nom})(1 - f_{ch}) + J(T_{ch})f_{ch}
\]

(11)

Figure 7 shows the result of this calculation normalizing the average particle flux to \( J(T_{nom}) \). The effect of the exponential response in vapor pressure is clearly visible in the figure. For instance, a PFC geometry with only 3.2% chamfer surface area and \( f_{enh} = 2.5 \) will experience a 40-fold increase in particle flux from the surface due to the local temperature peaking. As a result, experiments conducted on PFCs exhibiting leading-edge heating will require some careful interpretation as not only will the surface fluxes be larger than expected, these conditions may also be transient as some portions of the PFC-face exhibit an increased material loss from some regions and not others leading to inhomogeneous depletion.

5.2 Porous-MHD effects and surface replenishment

Both the CPS system and the divertor targets proposed by the NSTX-U group feature liquid metal flow through a porous material. The porous material is advantageous for fluid stability[27] and can provide a passive means of replenishing a surface. This is the phenomenon of porous material imbibition[33]. Flow through a porous material can be described
by the Darcy equation:

\[ u = \frac{k \Delta P}{\mu L} \quad (12) \]

where \( u \) is the fluid velocity, \( k \) is the permeability of the porous material, \( \Delta P \) is a pressure differential, \( \mu \) is the fluid viscosity and \( L \) is some distance over which \( \Delta P \) is present. In the case of a simple porous material and wetting liquid\(^1\) the pressure at the interface between the non-wetted and wetted portions of the porous material are given as the capillary pressure, \( P_C \):

\[ P_C = \frac{2 \Sigma \cos(\gamma)}{r_p} \quad (13) \]

where \( \Sigma \) is the surface, or interfacial, tension of the liquid, \( \gamma \) is the contact angle of the liquid on the porous substrate and \( r_p \) is the mean pore radius. In the case of a moving fluid of electrical conductivity, \( \sigma \), in an applied magnetic field, \( B \), an additional pressure drop over the length of moving fluid is approximated as:

\[ P_{MHD} \simeq -\sigma u B^2 L \quad (14) \]

\(^1\)A “wetting liquid” is here defined as one for which the contact angle is less than 90°.
An MHD version of the Lucas-Washburn equation is formed by including both capillary and MHD pressure terms in the Darcy equation and rearranging as:

\[
Lu = \frac{dL}{dt} = \frac{2\Sigma \cos(\gamma)}{r_p} \cdot \frac{1}{\mu/k + \sigma B^2}
\]  

(15)

Including a definition of the Hartmann number using the average pore radius as the characteristic length, \(Ha = r_p B \sqrt{\sigma/\mu}\), one can solve for the location of the wicking front as a function of time:

\[
L(t) = \left( \frac{4\Sigma r_p \cos(\gamma)}{\mu (r_{p}^2/k + Ha^2)} t \right)^{1/2} = S \sqrt{t}
\]

(16)

where \(S\) is known as the sorptivity of the porous-MHD system.

While instructive, more insight into the importance of the results associated with eq. 16 can be obtained. Returning to eq. 15, one can combine terms to create a modified definition of the Hartmann number taking into account the effectively enhanced viscosity due to the permeability of the porous material:

\[
\chi = \frac{k}{r_p^2} Ha^2
\]

(17)

where \(\chi\) is the permeability-enhanced Hartmann number. Using this definition, eq. 15 is rearranged to yield:

\[
L \frac{dL}{dt} = \left( \frac{2\Sigma \cos(\gamma)}{B \sqrt{\sigma \mu}} \right) \cdot \frac{\sqrt{k}}{r_p} \cdot \frac{\sqrt{\chi}}{1 + \chi}
\]

(18)

This form allows one to optimize a porous material for a given magnetic field and other fluid properties. This is done by maximizing the fluid flow which means finding the maximum of the function \(f(\chi) = \sqrt{\chi}/(1 + \chi)\). This is easily evaluated using basic calculus and the maximum is found to be obtained for a value of \(\chi = 1\). As with more conventional MHD problems, this optimization indicates that a maximum of flow is found at the point that the viscous drag is equal to the MHD drag for the particular geometry of the system. This is illustrated in figure 8.
As an illustration, a common approximation for the permeability of a packed-bed of spheres with porosity of $\epsilon = 0.5$ is estimated with the Kozeny-Carman equation\[33\]:

$$k = \frac{\epsilon^3}{45(1 - \epsilon)^2} r_p^2$$

with liquid lithium properties at 250°C and a field of 1 T. This would indicate an optimal pore size of about 130 $\mu$m.

The MHD effects create an anisotropic sorptivity even if the porous material is isotropic throughout. In the directions perpendicular to the magnetic field, the MHD damping reduces the flow rate while parallel to the magnetic field only viscous drag occurs. As a result one can evaluate the sorptivity for the parameters above and find that $S^2_{\perp} = 16$ cm$^2$s$^{-1}$ and $S^2_{\parallel} = 38$ cm$^2$s$^{-1}$. These values have a practical impact on the design of prefilled or fully flowing PFCs of the variety that have oozing pores communicating material from a reservoir or internal pipe of lithium. Equation 16 can be rearranged such that a characteristic time, $\tau_{\text{replenish}}$ to
replenish a surface over the distance between pores, $L_{\text{pore}}$ can be calculated:

$$\tau_{\text{replenish}} = \frac{L_{\text{pore}}^2}{S^2} = \frac{1}{f_{\text{replenish}}}$$  \hspace{1cm} (20)

where a replenishing frequency, $f_{\text{replenish}}$ can be taken from the characteristic time. For a characteristic scale length of 1 cm the replenishment frequency is in the range of 16-38 Hz depending on parallel or perpendicular flow for the optimal pore size in a 1 T field. This range of frequencies is already close to the typical ELM frequency in tokamak devices so that if an ELM event were severe enough to completely ablate all the surface lithium, the wicking process would be expected to recover the surface prior to the next ELM event.

6 Summary

The potential benefits of liquid metal, and in particular liquid lithium, plasma-facing components has been re-iterated. The NSTX-U program has a particular focus on making a critical assessment of the conventional high-Z wall approach alongside the low-Z, liquid metal PFC approach in a single device. Of particular importance in establishing the feasibility of liquid lithium as a fusion PFC is determining the operating temperature window. In the area of power-exhaust capacity, the maximum temperature compatible with good core confinement could have significant impact on the direction of development for future liquid metal PFCs.

The NSTX-U is well suited to testing liquid metal PFCs due to the large heating power available as well as the flexible magnetic configurations. A three-step upgrade path has been described that will address the key elements required to implement fully-flowing liquid lithium PFCs in the NSTX-U beginning with the high-Z divertor upgrade. Scientific and technological progress will be made at each upgrade. Two specific issues are given to illustrate some of the research questions associated in these first two steps.

In the NSTX-U high-Z divertor upgrade, leading edges will be mitigated with the use of a chamfer shaping at the tile edges. The geometric construction of these chamfers was
described. While the increase in average surface temperature is nearly trivial to evaluate, a significant increase in surface particle flux is expected due to the exponential response of the lithium vapor-pressure to the surface temperature. The pre-filled liquid metal target has been described in concept. A key question for this and other concepts utilizing a porous medium is how to account for the effects of MHD drag inside a porous material. An analysis is presented deriving an MHD-modified Lucas-Washburn equation which results in anisotropic sorptivities. The sorptivity can be maximized, however, to provide the fastest possible wicking through the material. Replenishment rates from reasonably sized pores are commensurate with typical ELM cycle times indicating rapid replenishment of liquid metals is feasible even inter-ELM.

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